



Microstructural Degradation of Ni/YSZ Electrodes in Solid Oxide Electrolysis Cells under High Current

Chen, Ming; Liu, Yi-Lin; Bentzen, Janet Jonna; Zhang, Wei; Sun, Xiufu; Hauch, Anne; Tao, Youkun; Bowen, Jacob R.; Hendriksen, Peter Vang

Published in:
Journal of the Electrochemical Society

Link to article, DOI:
[10.1149/2.098308jes](https://doi.org/10.1149/2.098308jes)

Publication date:
2013

Document Version
Peer reviewed version

[Link back to DTU Orbit](#)

Citation (APA):
Chen, M., Liu, Y.-L., Bentzen, J. J., Zhang, W., Sun, X., Hauch, A., Tao, Y., Bowen, J. R., & Hendriksen, P. V. (2013). Microstructural Degradation of Ni/YSZ Electrodes in Solid Oxide Electrolysis Cells under High Current. *Journal of the Electrochemical Society*, 160(8), F883-F891. <https://doi.org/10.1149/2.098308jes>

General rights

Copyright and moral rights for the publications made accessible in the public portal are retained by the authors and/or other copyright owners and it is a condition of accessing publications that users recognise and abide by the legal requirements associated with these rights.

- Users may download and print one copy of any publication from the public portal for the purpose of private study or research.
- You may not further distribute the material or use it for any profit-making activity or commercial gain
- You may freely distribute the URL identifying the publication in the public portal

If you believe that this document breaches copyright please contact us providing details, and we will remove access to the work immediately and investigate your claim.

Microstructural degradation of Ni/YSZ electrodes in solid oxide electrolysis cells under high current

Ming Chen ^{*}, Yi-Lin Liu, Janet Jonna Bentzen, Wei Zhang, Xiufu Sun, Anne Hauch, Youkun Tao, Jacob R. Bowen, Peter Vang Hendriksen

Department of Energy Conversion and Storage, Technical University of Denmark,
DK-4000 Roskilde, Denmark

^{*} minc@dtu.dk

Abstract

Ni/yttria stabilized zirconia (YSZ) supported solid oxide electrolysis cells (SOECs) were exposed to long-term galvanostatic electrolysis tests, under different testing conditions (temperature, gas composition, current density etc.) with an emphasis on high current density (above -1 A/cm^2). Detailed post-mortem characterizations were carried out to investigate microstructural changes after long-term galvanostatic tests, focusing on the Ni/YSZ electrode. Formation of ZrO_2 nano-particles on Ni surfaces was observed in cells exposed to -1 or -1.5 A/cm^2 at 800 or 850°C , but not in those tested at current densities below -0.75 A/cm^2 . The formation of ZrO_2 nano-particles deteriorates Ni percolation and presumably decreases the number of active triple phase boundaries (TPBs) and is therefore considered a degradation phenomenon. It is hypothesized that the degradation of the Ni surface is a result of Ni-YSZ interfacial reactions, taking place under the conditions prevailing under strong polarization. A mechanism for the formation of ZrO_2 nano-particles on the Ni surface

under the electrolysis cell testing is proposed and the possibility of Ni-YSZ interfacial reactions under such conditions ($T, p(\text{O}_2)$) is further elucidated by thermodynamic calculations.

Introduction

Over the past decade, there has been an increased interest in development of solid oxide electrolysis technology for hydrogen or synthesis gas ($\text{CO} + \text{H}_2$) production. In solid oxide electrolysis cells (SOECs), electrical energy can be converted to chemical energy and stored as H_2 or synthesis gas via high temperature electrolysis of steam or co-electrolysis of steam and CO_2 [1, 2]. For SOECs to become commercially interesting, durability is one of the critical issues. Long-term stability for 5-10 years of operation is generally required [3, 4]. In addition, it is advantageous to operate SOECs at high current density in order to decrease production cost and to achieve high H_2 or synthesis gas production rate.

Several studies of long-term durability of SOECs have been reported in literature and different degradation mechanisms have been observed [2, 5-7]. The suggested degradation mechanisms include segregation of impurity phases (from raw materials or from sealing materials) to the triple phase boundary (TPB) [5], poisoning of Ni/yttria stabilized zirconia (YSZ) electrodes by impurities from the gas stream [2], and oxygen electrode delamination or crack formation within the YSZ electrolyte due to high oxygen activity at the electrolyte-oxygen electrode interface [6]. For SOECs operated at low current density (below -1 A/cm^2), it has been reported that impurity poisoning of the Ni/YSZ electrode is the main cause for degradation. By cleaning inlet gas to the Ni/YSZ electrode and using alternative seals with minimum emission, almost zero degradation has been demonstrated [8]. At current densities above -1 A/cm^2 , oxygen electrode delaminates or lateral

cracks form within the YSZ electrolyte, causing an additional, rather severe and irreversible degradation process [6]. On the other hand, the Ni/YSZ electrode degradation was ascribed to a consequence of absorbed impurities, but no direct relation with the applied current density was reported. It is likely that the electrode polarization and the established $p(\text{O}_2)$ at the electrodes is a more determining parameter for the degradation. However, this is not a controlled quantity and is not known accurately in all cases. Hence, results are here grouped according to current density.

In the present work, we present results on post-mortem analysis of Ni/YSZ electrodes exposed to long-term galvanostatic electrolysis tests, under different testing conditions (temperature, gas composition, current density etc.) with the emphasis on high current density (above -1 A/cm^2). The temperature of operation was 800 or 850 °C. Detailed post-mortem characterizations utilizing scanning electron microscopy (SEM) and energy dispersive X-ray spectroscopy (EDS) were carried out to investigate microstructural changes after long-term durability tests. A new degradation mechanism of the Ni/YSZ electrode is reported, which interprets the observed dependence of the microstructural changes on the current density, or more precisely, the electrode over-potential. Thermodynamic calculations were carried out to further elucidate the suggested mechanism.

Experimental

Electrochemical testing

Table 1 summarizes the cell test conditions. Except for the Ref2 cell, all the other studied cells (A1-A8 and Ref1) have a Ni/YSZ support, a Ni/YSZ active electrode (as the cathode in SOEC mode), a YSZ electrolyte and a LSM/YSZ composite oxygen electrode (as the anode; LSM: strontium doped

lanthanum manganite). The Ref2 cell differs from the others only by having a LSCF/CGO (LSCF: strontium doped lanthanum cobalt ferrite, CGO: gadolinia doped ceria) oxygen electrode with a CGO barrier layer between the electrolyte and the oxygen electrode. The Ref2 cell is acceptable for use as a reference since the focus of the present study is on the Ni/YSZ electrode side. The details of cell fabrication can be found elsewhere [9]. The electrochemical performance of the cells was characterized via single cell testing (A1-A5, A7-A8, Ref1, and Ref2) or stack testing (A6). All the cells were reduced and subjected to initial performance characterization by measuring DC polarization (i-V) curves and/or AC electrochemical impedance spectra (EIS), then followed by long-term durability tests, but no long-term testing was performed for the two reference cells (Ref1 and Ref2). The long-term tests were carried out under galvanostatic conditions, i.e. constant current density in the range from -0.5 to -1.5 A/cm². Both steam electrolysis (50% H₂O + 50% H₂) and co-electrolysis of steam and CO₂ (45% CO₂ + 45% H₂O + 10% H₂), with a gas (H₂O + CO₂) conversion from 28% to 80% (based on Faraday's law) were investigated.

Post mortem analysis

Both fractured and polished cross-sections were prepared from the studied cells. A Supra 35 scanning electron microscope from Carl Zeiss was used, which is equipped with a field emission gun (FE-SEM) for obtaining high resolution and high contrast specifically in low voltage applications. For chemical analysis the Supra 35 is equipped with an X-ray Energy Dispersive Spectrometer (EDS) and a microanalysis software NSS (Thermo Fischer Scientific Inc.). To ensure that observed microstructure patterns are representative, at least three locations of each cell were inspected: inlet, middle, and outlet with respect to gas to the Ni/YSZ electrode. For all the long-term tested cells, the observed microstructural changes are more pronounced at the gas inlet and

middle of the cell than at the outlet. Due to length limitation, SEM results from different locations are presented here only for Cell A4. For all other studied cells, only results from center of the cells are presented.

For the fractured samples a low accelerating voltage of 5 kV was used which allowed direct imaging of the fractured surface without carbon coating. Combined with usage of a short working distance of 4-5 mm, the surface morphology could be examined on a nano-meter scale. With the aim of increasing sensitivity of surface chemical analysis, a low accelerating voltage of 5 kV was applied also for EDS analysis, which resulted in a X-ray penetration depth of around 200 nm. However, it should be kept in mind that EDS results obtained from irregular fractured surfaces have to be interpreted with precautions. They can only be of a qualitative value even in the best case.

The polished cross-section samples were used firstly to examine the percolation of Ni in the Ni/YSZ electrodes. For this purpose no carbon coating was applied and a low-voltage (< 1 kV) charge contrast technique [10] and the Inlens secondary electron detector in the SEM were used. The samples were then carbon coated for SEM imaging and EDS analysis at an accelerating voltage of 15 kV.

Cell A4 was selected for further study by transmission electron microscopy (TEM). A small piece from the center of the cell was mechanically polished to a thickness of approximately 20 μm . Final thinning to < 100 nm thickness was done by focused ion beam (FIB) milling at 10-20 pA probe current using a 1540 XB FIB SEM from Carl Zeiss operated at 30 kV. Final polishing in the FIB was performed at 5 kV in order to reduce the amorphous surface layer and Ga-ion implantation. A

JEM-3000F microscope (JEOL, Japan) equipped with a field-emission gun operated at 300 kV was employed for high-resolution TEM (HRTEM) analysis. The point resolution of the TEM is 0.19 nm.

Results

Cell degradation

Details on the performance, durability, and degradation of the cells are reported in [5, 11-13]. Figure 1 presents a plot of cell voltage evolution with time during long-term galvanostatic testing. Among the eight long-term tested cells, Cells A5, A7 and A8 were tested applying steam electrolysis at 850 °C and -1.5 or -0.5 A/cm², while the other five cells were tested applying co-electrolysis of steam and CO₂ at a temperature of 800 or 850 °C and a current density of -0.75, -1 or -1.5 A/cm². For Cell A6, which is one of the eleven cells tested in a stack [11], the measured voltage represents the contribution over an entire single repeating unit (SRU, including cell, interconnect, and contact between the cell and interconnect). The interconnect plate contact resistance was reported to be around 0.10 Ω cm² (800 °C), corresponding to a voltage loss of 75 mV at -0.75 A/cm². The actual cell voltage will therefore be about 75 mV lower than the measured SRU voltage. The OCV and final cell voltage for the eight tested cells are further listed in Table 1. The cell over-potential at the end of electrolysis testing is then calculated as “Final cell voltage – OCV” and also given in Table 1. For Cell A6, two values are provided: one over the SRU (actually measured) and the other corrected for the interconnect plate contact resistance. At the end of the durability tests, the cells reached a voltage ranging from 1116 mV (A8) to 1772 mV (A1), corresponding to a cell over-potential ranging from 161 mV (A8) to 900 mV (A1).

SEM observations

In the present work, both the fractured and polished cross-sections of the cells were examined using SEM and EDS, with a focus on the active Ni/YSZ electrode. Due to a large number of cells to be examined, a careful selection of the cells for different post-mortem characterization schemes (fractured or polished cross-sections) was carried out. The fractured cross-section is ideal for investigating morphology changes of Ni or YSZ grains, while the polished one is more suitable for investigating Ni percolation and for EDS analysis. A short summary of main findings from post-mortem characterizations of the Ni/YSZ electrodes is listed in Table 2.

Fractured surfaces

The fractured surfaces of the three tested cells A3, A4, and A8 as well as a reference cell Ref2 were examined. Cells A2 (-1.5 A/cm^2 , $800 \text{ }^\circ\text{C}$) and A3 (-1.5 A/cm^2 , $800 \text{ }^\circ\text{C}$) were tested under the same conditions for almost same period of time. The two cells show similar microstructure degradation pattern. Also the cells showed very similar electrical degradation pointing to a good reproducibility of the results. In this paper, only the SEM results from Cell A3 are presented. Figure 2 shows details of the active Ni/YSZ electrode microstructure at different magnifications. High resolution SEM of the fractured surfaces revealed nano-particles covering a major part of the Ni grains closest to the interface between the Ni/YSZ active electrode and the YSZ electrolyte in Cells A3 (-1.5 A/cm^2 , $800 \text{ }^\circ\text{C}$) and A4 (-1 A/cm^2 , $850 \text{ }^\circ\text{C}$), being more pronounced in Cell A4. As illustrated in Figures 2b-d, the formation of nano-particles was a general feature over the entire cell for Cell A4, though the abundance of the nano-particles differs among the three inspected locations, being more abundant at the inlet and center than at the outlet. This is also true for the other long-term tested

cells at -1.5 A/cm^2 (such as Cell A3). Here only the SEM image from the center is presented (Figure 2a) due to space limitation. The size of these particles varies from around 10 to 100 nm. These nano-particles appear on the Ni grain surface, which was originally in contact with pores, or YSZ grains, or other Ni grains. In the two latter cases, the formation of these nano-particles will obviously introduce detachment of Ni-Ni or Ni-YSZ interface. This type of nano-particles was not found on the Ni grains farther away from the interface and in the support. For the cells tested at -0.5 A/cm^2 (A7 and A8) and Cell Ref2, formation of nano-particles on Ni grains was not found.

Figure 3 shows EDS point analyses on Ni and YSZ grain surfaces in Cell A4 (-1 A/cm^2 , 850°C) and Cell Ref2. With a working distance of 13 mm for EDS analysis and an accelerating voltage of 5 kV, the signal intensity (i.e. the signal-to-noise ratio) is rather low. However, qualitatively the EDS point analyses provide the information that the nano-particles (Point 3 in Figure 3a) contain high amounts of Zr and O, indicating that these nano-particles might be Zr-oxide. Note that in the reference cell (Cell Ref2), individual particles can be clearly identified as either YSZ or Ni. “Effectively” intermediate compositions like Point 3 in Figure 3a are not observed in Cell Ref2.

In addition, TEM analysis of Cell A4 has confirmed that these nano-particles (as illustrated by the arrows in Figure 4a) are Y-containing ZrO_2 . Figures 4b and 4c show two representative HRTEM images, corresponding to the yellow and cyan circled areas in Figure 4a. By measuring the inter-planar lattice spacing of local areas in the inverse Fast Fourier Transform (IFFT) images (Figures 4b and 4c insets) where characteristic crystal planes of cubic or tetragonal ZrO_2 phases are well identified, one can confirm that the nano-particles are cubic or tetragonal zirconia. Figure 4d further gives EDS point analysis of the characteristic areas: Points 1, 2 and 3 in Figure 4a, corresponding to bulk YSZ, Ni-YSZ interface, Ni-pore interface respectively. A variety of Zr/Y atomic ratios from

the bulk YSZ (Zr/Y=4.3) to the Ni-YSZ (2.8) or Ni-pore (6.4) interface was detected, indicating a mechanism of dissolution – diffusion – exsolution or precipitation accounting for the formation of the ZrO₂ nano-particles.

Polished surfaces

Polished samples of the cells A1 (-1.5 A/cm², 800 °C), A5 (-1.5 A/cm², 850 °C), A6 (-0.75 A/cm², 800 °C) and Ref1 were examined initially for evaluating Ni percolation. In the images obtained by the low-voltage contrast technique (Figure 5), significant loss of Ni percolation in the active electrode can be seen in the first two cells A1 and A5 as compared with the reference cell, whereas the Ni percolation in the active electrode is practically intact for the cell A6 tested at -0.75 A/cm² (Figure 5c).

In the SEM image of a polished cross-section, the Ni grain surfaces in contact with pores, or YSZ grains or other Ni grains are displayed as Ni-pore, Ni-YSZ or Ni-Ni interfaces, respectively. Therefore, variations of these interfaces observed in the polished sample of tested cells are indications of microstructural changes occurred on the surface of Ni grains, which are shown in Figure 6. It appears that in Cell A1 (-1.5 A/cm², 800 °C) and Cell A5 (-1.5 A/cm², 850 °C), new interfacial phases or gaps of a hundred nm or less in thickness are formed, which look like dark rings (continuous or discontinuous) around Ni (Figure 6a and b). In some cases a narrow region of a collection of nano-particles can be seen at Ni interfaces (Figure 6b). On the other hand, the Ni interface in Cells A6 (-0.75 A/cm², 800 °C) and A8 (-0.5 A/cm², 850 °C) is practically as clean as that in the reference cell Ref1 (Figure 6e). In addition to changes at the interface, inclusions inside Ni grains were found in Cell A5, which appear as black dots in Figure 6b.

Figure 7 shows a SEM image and EDS line-scan crossing an interfacial region containing nano-particles between two Ni particles in Cell A5 (-1.5 A/cm^2 , 850°C). The line-scan profile shows that the interface region contains Zr, O and very little Y (close to the detection limit for SEM/EDS) besides Ni. It has to be noted that the object is too small (the interface region is less than $0.5 \mu\text{m}$ in width) for a proper quantitative EDS analysis. However, the line-scan results do yield qualitative information indicating that the nano-particles on the surface of Ni are Zr-oxide particles.

EDS point analysis was also performed in the interior of relatively large Ni grains (with a diameter of at least $1 \mu\text{m}$) in the active Ni/YSZ electrode. Typical results are given in Table 3. Substantial concentrations of Zr and Si are detected within the Ni grains in the active layer. The Si content decreases sharply with increasing distance (up to $2\text{-}3 \mu\text{m}$) from the interface with the electrolyte while no significant changes of the Zr content are found within these few microns. As shown in Figure 6b and Figure 7a, Si-oxide precipitates as dark round spots (100 nm or less) within the Ni grains which are close to the electrode-electrolyte interface. The EDS line-scan (Figure 7b) evidences that the dark spot contains Si and O.

The SEM observations on the fractured and polished samples analyzed in this work are largely consistent with each other: In the active Ni/YSZ electrode, 1) nano-particles are formed on the surface of Ni grains in contact with YSZ grains, or other Ni grains, or pores, and 2) these nano-particles contain Zr and O, i.e. Zr-oxide. SEM observations shown in Figure 6 further reveal that the interface variations are more significant in the cells tested at higher current density (equal to or above -1 A/cm^2 , such as in Cell A1/A2/A3/A4/A5) than at lower current density (below -1 A/cm^2 , such as in Cell A6/A7/A8), suggesting that these interfacial reactions are associated with the

electrochemical processes during ageing. These variations are also more significant for the cells tested for longer time and/or at higher temperature (Cell A4: -1 A/cm^2 , 850°C and Cell A5: -1.5 A/cm^2 , 850°C). The SEM observations strongly suggest that formation of nano-particles on Ni surfaces is a degradation process of the Ni/YSZ electrode. Because it introduces detachment of Ni-Ni and Ni-YSZ interfaces, weakens or blocks the electric contact between Ni grains or between Ni and YSZ grains, deteriorates Ni percolation and presumably decreases active TPB. Similar phenomena were recently reported by Tietz et al. [14]. They carried out detailed post-mortem characterizations on a Ni/YSZ electrode supported cell operated for steam electrolysis at 800°C and -1 A/cm^2 for 9000 hours. Formation of nano-particles on Ni surfaces in the active Ni/YSZ electrode is clearly shown in Figure 8a of their paper. However, no detailed account of the underlying mechanism is shown.

Discussion

Mechanism for formation of ZrO_2 nano-particles

Electrochemically induced ZrO_2 reduction at the Ni- ZrO_2 interface has been previously reported [15-17]. At very low oxygen partial pressures the Ni- ZrO_2 interface is thermodynamically unstable. Therefore, intermetallic phases Ni_xZr_y may form at the interface under low oxygen activity. On the other hand, Ni_xZr_y may be oxidized forming Ni and ZrO_2 at the interface with high oxygen activity. This type of process occurs at very low oxygen partial pressure (see below) and is not realistic under the present cell test condition.

In the present work we hypothesize a slightly different mechanism which is illustrated in Figure 8. During SOEC testing, the over-potential at the Ni-YSZ interface results in a local interface region

with a decreased oxygen partial pressure, under which Zr atoms at the Ni-YSZ interface start to dissolve into the metallic Ni phase. The Zr then diffuses via the bulk or surface of Ni (Figure 8, green dashed lines) and precipitates as ZrO_2 somewhere else where $\mu(\text{O}_2)$ (or $p(\text{O}_2)$) is higher and the chemical potential of Zr - $\mu(\text{Zr})$ is lower, for example, at the interface between Ni-Ni or between Ni-pore. Though we have no evidence to exclude diffusion of Zr via the Ni grain surface, it is most likely that ZrO_2 nano-particles formed at the Ni-Ni or Ni-pore interface were induced by Zr bulk diffusion through Ni.

Thermodynamics of Ni-Zr-O

In this work, thermodynamic calculations were carried out to further elucidate the proposed mechanism. To calculate the reactions at the Ni-YSZ interface, a thermodynamic database of Ni-Y-Zr-O is required which is still under development by the present authors. Instead, a semi-quantitative discussion based on thermodynamic calculations of the Ni-Zr-O system using FACTSAGE Thermochemical Software and Databases [18] is presented here.

The calculations are based on thermodynamics of NiO, cubic ZrO_2 , and the metallic phases in Ni-Zr. Eight intermetallic compounds (Ni_5Zr , Ni_7Zr_2 , Ni_3Zr , $\text{Ni}_{21}\text{Zr}_8$, Ni_4Zr_3 , $\text{Ni}_{11}\text{Zr}_9$, NiZr , and NiZr_2) exist in the Ni-Zr system. Besides, the metallic Ni phase (FCC) can dissolve less than 2 mol.% Zr. However, there is no experimental evidence to confirm a particular value. Metallic Zr has two polymorphs, a low temperature HCP phase with almost zero Ni solubility and a high temperature BCC phase with a few mole percent Ni solubility. The interaction between NiO and ZrO_2 is rather limited. No complex oxide exists in the NiO- ZrO_2 system. A few studies have been carried out to examine the solubility of NiO in ZrO_2 and a solubility limit of from 2 to 20 mol.% NiO in cubic or

tetragonal ZrO_2 was reported by different groups [19-21]. The discrepancy could be partially attributed to the fact that stabilization of ZrO_2 depends on its surface to volume ratio [22], i.e. below the critical particle size for monoclinic ZrO_2 formation, tetragonal or cubic ZrO_2 can be stabilized. However, high temperature treatment may still destabilize tetragonal or cubic ZrO_2 . The above mentioned studies may just represent a picture of metastable equilibrium in NiO-ZrO_2 . It is still questionable if NiO alone can actually stabilize tetragonal or cubic ZrO_2 at high temperature without any other dopant such as Y_2O_3 . The solubility of ZrO_2 in NiO was reported to be negligible at 1600°C by Chang et al. [23]. In this work, no interaction between NiO and ZrO_2 is considered.

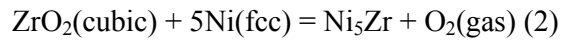
Figures 9 and 10 present phase diagrams of Ni-Zr-O_2 at 850°C . According to the calculations, with decreasing oxygen partial pressure at the Ni-ZrO_2 interface, Zr from ZrO_2 starts to dissolve into metallic Ni . To estimate at which $p(\text{O}_2)$ this process occurs, a limiting Zr content in the metallic Ni phase needs to be specified. The equilibrium oxygen partial pressure can then be back calculated. Here 1 ppm of Zr in the metallic Ni phase was assumed as the limiting content. This translates into an equilibrium oxygen partial pressure of 3.2×10^{-29} bar. When the oxygen partial pressure is below 3.2×10^{-29} bar, the equilibrium concentration of Zr in metallic Ni is higher than 1 ppm. This can be further expressed as the reaction below:



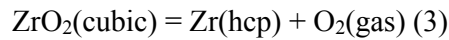
It is reasonable to assume that the process of Zr dissolving into Ni at the Ni-ZrO_2 interface starts at a $p(\text{O}_2)$ equal to or lower than 3.2×10^{-29} bar. With decreasing oxygen partial pressure, the solubility of Zr in Ni increases and reaches a maximum of 0.5 mol.% at 850°C . The dissolved Zr may further diffuse and precipitate somewhere else where $p(\text{O}_2)$ is higher and form ZrO_2 . The

oxygen solubility in Ni is rather small, below 0.05 mol.% which is only one tenth of the maximum Zr solubility in Ni [24]. The kinetics of Zr diffusion in Ni is yet unknown. However, a rough idea can still be obtained by using the kinetics of Hf diffusion in Ni. The intrinsic diffusivity of Hf in Ni has been measured to be in the order of 10^{-12} cm²/s at 850°C [25], corresponding to a diffusion distance of ~ 1 μ m in one hour. The kinetics of oxygen diffusion in Ni is much faster than that of Zr and is in the order of 10^{-9} cm²/s at 850°C [26], corresponding to a diffusion distance of ~ 40 μ m in one hour. It is reasonable to assume that ZrO₂ will most probably precipitate at the Ni-Ni or Ni-pore interface, though a possibility of ZrO₂ precipitation inside Ni grains cannot be totally ruled out.

As shown in Figure 9, at $p(\text{O}_2) \leq 10^{-33}$ bar, various intermetallic compounds form at the Ni-ZrO₂ interface, in equilibrium with metallic Ni on one side and ZrO₂ on the other. The reaction for formation of Ni₅Zr can be written as:



This process corresponds to the observations reported by Wagner et al. [15-16] and Klotz et al. [17]. When $p(\text{O}_2)$ is below 1.3×10^{-41} bar, ZrO₂ is no longer stable and is reduced into metallic Zr (hcp).



Based on the above calculations, it is clear that stability of ZrO₂ in contact with Ni is strongly reduced as compared to pure ZrO₂, i.e. the reduction $p(\text{O}_2)$ of ZrO₂ is increased from 1.3×10^{-41} bar (pure ZrO₂) to 3.2×10^{-29} bar (ZrO₂ in contact with Ni).

It should be emphasized that the thermodynamics for Reactions (1) and (2) has not been experimentally validated. The reliability of the calculated critical $p(\text{O}_2)$ for the above calculations relies on the reliability of the Gibbs energy functions. A difference of 50 kJ/mol in the Gibbs energy, which is within a normal uncertainty range for measured enthalpy, can result in a difference of 3 decades in the calculated critical $p(\text{O}_2)$. For example, Wagner et al. [16] claimed that Reaction (2) takes place at 10^{-27} bar at 1200 K, while FACTSAGE gives 10^{-30} bar. The calculated critical $p(\text{O}_2)$ in the present work shall therefore be interpreted bearing in mind this uncertainty, such as $3.2 \times 10^{-29 \pm 3}$ bar for Reaction (1) at 850 °C.

With respect to influence of yttrium, the solubility of yttrium in Ni was reported to be 0.1 mol.% at 1523 K and effectively zero at lower temperature [27]. NiO and Y_2O_3 do not react with each other and the mutual solubility is negligible. According to the thermodynamics of the Y-Zr-O system, the presence of yttria in YSZ at the Ni-YSZ interface may have some influence on the Zr dissolving process, but not in a significant way. The above calculations can be applied to the Ni-YSZ interface fairly well. However, a validated thermodynamic database of Ni-Y-Zr-O is still valuable in order to clarify the reactions at the Ni-YSZ interface.

Over-potential at the Ni-YSZ interface

In this section we analyze the over-potential at the Ni-YSZ interface to see if it is likely that conditions that predict Zr reduction are reached.

According to the Nernst equation, the oxygen partial pressure at the Ni-YSZ interface in an operating SOEC cell is determined by local gas composition and over-potential (voltage loss between OCV and cell voltage under current) over the Ni-YSZ interface:

$$\eta_{\text{Ni/YSZ}} = R \times T \times \ln(p(\text{O}_2)_{\text{Local gas}}/p(\text{O}_2)_{\text{Ni/YSZ}})/(4 \times F) \quad (4)$$

Where R is the gas constant and F is Faraday's constant. This is further illustrated in Figure 11. Here over-potential is used for discussion instead of $p(\text{O}_2)$, in order to be better correlated with measured cell voltages. As for Cell A5 (-1.5 A/cm^2 , 850°C , Figure 11a), in order to reach a critical $p(\text{O}_2)$ of $3.2 \times 10^{-29 \pm 3}$ bar at the Ni-YSZ interface, an over-potential of $625 \pm 167 \text{ mV}$ is required with reference to a local gas composition of $50\% \text{ H}_2\text{O} + 50\% \text{ H}_2$ (i.e., no gas conversion, $p(\text{O}_2) = 5.3 \times 10^{-18}$ bar). Local gas composition changes, which are caused by conversion of steam into hydrogen, can contribute 106 mV at 80% conversion and 177 mV at 95% conversion. The remaining shall be contributed by the cathode polarization - $\eta_{\text{Ni/YSZ}}$, which is estimated from the measured cell voltages in this work. For actual $\eta_{\text{Ni/YSZ}}$, an average value over the entire cell could be determined by equivalent circuit modeling of the measured impedance spectra, assuming that various electrochemical processes can be well separated. For the cell type (Ni/YSZ cathode, YSZ electrolyte, and LSM/YSZ anode) tested here, the cathode part of the cell resistance is initially 20% of the total cell resistance for steam electrolysis, $40\text{-}50\%$ for CO_2 electrolysis, and in between for co-electrolysis [5, 28, 29]. Hauch et al. reported that the cathode part of the cell resistance was increased from $\sim 20\%$ of the total cell resistance to $\sim 30\%$ after $500\text{-}1200$ hours testing at -0.5 A/cm^2 and 850°C [5]. In some incidents the degradation at the cathode is much stronger than at the anode [13]. It could be expected that the cathode constitutes a much higher percentage of the total resistance (or the total cell over-potential) after long-term testing at -1 or 1.5 A/cm^2 . It is rather

difficult to determine local $\eta_{\text{Ni/YSZ}}$, as it is dependent on a number of factors such as local gas composition and local current distribution. In this work, we simply assume the local $\eta_{\text{Ni/YSZ}}$ to be 1/3-2/3 of the total over-potential over the entire cell measured at the end of durability tests. This is at least in specific cases a sound assumption according to previous investigations [5, 13, 28-29].

As shown in Figure 11, if one assumes that ~40% of the cell over-potential in Cell A5 (-1.5 A/cm², 850 °C) is due to the Ni/YSZ cathode, it is strong enough to lead to reduction of ZrO₂ at the ZrO₂-Ni interface. For Cell A3 (-1.5 A/cm², 800 °C), one has to assume that 55% of the total cell over-potential occurs at the cathode to reach the estimated level for the ZrO₂ reduction (not shown here). As discussed in the previous paragraph, in some cases, the cathode polarization can indeed constitute such large part of the total cell over-potential, though in general for this type of cell it is not that dominant. For Cells A1 and A2, conditions are similar to A3 and A5. For all these cells formation of ZrO₂ nano-particles on Ni grain surfaces was observed. For the cells where this was not observed (A6-A8), polarizations are much smaller, and the $p(\text{O}_2)$ at the Ni-YSZ interface does not reach the level needed for ZrO₂ reduction at the interface.

It is clear that there is a strong correlation between formation of ZrO₂ nano-particles and polarization; the ZrO₂ nano-particles only formed close to the interface and only in the strongest polarized cells. The semi-quantitative assessment attempted above indicates that in the case of a strong domination of cathode polarization, one can reach sufficiently reducing conditions to reach the level estimated from the calculated phase diagrams. However, the correlation between estimated polarizations and observed microstructural changes is not fully consistent. Cell A4 (-1 A/cm², 850 °C), where also ZrO₂ nano-particles were formed, was not polarized to an extent where conditions can reach the predicted threshold. It is suggested that the reason for this lies in an uncertainty of the

required $p(\text{O}_2)$ for the reduction. An effort to determine reduction potential of ZrO_2 on Ni is underway.

It should be mentioned that the critical $p(\text{O}_2)$ for Reaction (2) is 10^{-33} bar at 850 °C, being four decades lower than that for Reaction (1). It is most unlikely that the $p(\text{O}_2)$ at the Ni-YSZ interface in the here tested cells will reach the threshold allowing for Reaction (2) to take place. It is however difficult to totally rule out the possibility due to large uncertainty associated with the thermodynamics.

Also Si can be reduced and dissolved in the Ni grains in a reaction analogue to Reaction (1). It is well established that silica is present as an impurity in the Ni/YSZ materials [5, 30]. Besides, Si from glass seal evaporates in highly humidified atmospheres and is transported via the gas stream in a form of $\text{Si}(\text{OH})_4$, and finally deposits at the triple phase boundary of the Ni/YSZ electrode [5]. The minimum over-potential required for Si from SiO_2 dissolving into Ni at 850 °C is calculated as 170 mV. This is totally realistic for Ni/YSZ electrode under high electrolysis current (see Table 1). After the cell is returned to OCV, the dissolved Si may be oxidized again as a SiO_2 inclusion. This explains the phenomena observed in Cell A5 (-1.5 A/cm^2 , 850 °C, Figures 5 and 6). In addition, a clear relation between Si inclusion and distance to the glass seal has been confirmed (not presented in this paper); the closer to the glass seal, the more SiO_2 inclusions. This further supports our proposed mechanism.

Summary

In this work, formation of ZrO_2 nano-particles on Ni grains was observed in the active Ni/YSZ electrode, only in the region close to the cathode-electrolyte interface, i.e. where one will find the most reducing conditions in the Ni/YSZ electrode during electrolysis testing. The ZrO_2 nano-particles are observed in cells tested at current density equal to or above -1 A/cm^2 , but not in non-tested cells or cells tested at lower current density. The harsher the conditions (in terms of cathode polarization, temperature, and testing period), the larger the abundance of the ZrO_2 particles.

It is emphasized that Zr reduction may occur at a much higher $p(\text{O}_2)$ in the presence of Ni than when in pure ZrO_2 (or YSZ) form. The threshold value is around $3.2 \times 10^{-29\pm3}$ bar at 850°C , assuming an error range of 50 kJ/mol for ΔG of Reaction (1). The observation of a clear correlation with cathode polarization and the observation of a variety of Zr/Y ratios from the bulk YSZ to the ZrO_2 nano-particles formed at the Ni-YSZ or Ni-pore interface support qualitatively the formulated hypothesis for the formation mechanism being a reduction, followed by solid diffusion and re-precipitation at sites with higher $p(\text{O}_2)$.

However, the correlation between estimated polarizations and observed microstructural changes is not fully consistent. The reason for the discrepancy is ascribed to an uncertainty of the required $p(\text{O}_2)$ for the reduction. It should be noted that considerable uncertainty is associated both with the assessments of local $p(\text{O}_2)$ in the experiments and the calculated thresholds. The predicted $p(\text{O}_2)$ rely on an assumption of how the degradation is distributed over the cell and an assumption that the cathode contributes 40-60% of the total cell resistance when tested at current density above -1 A/cm^2 . This is estimated from other tests but not measured directly on the here tested cells. A large uncertainty however is associated with the thermodynamics of the interface reactions. Firstly this could be inaccurately determined. Secondly its value could be somehow affected by special

conditions relevant to the tests here. For example, presence of Si could somehow reduce the Zr stability or the reduction potential could be affected by Ni particle size or presence of non-identified secondary phases. We are currently trying to measure directly the decomposition potential of ZrO_2 on Ni to obtain a better quantitative assessment of this, which could allow a quantitative proof or disproof of the hypothesis and strengthen the more quantitative arguments presented here.

Conclusions

This is a report of post-mortem analyses of a number of SOECs tested under both co-electrolysis and steam electrolysis conditions at 800-850°C with current density ranging from -0.5 to -1.5 A/cm². An important microstructural degradation of the Ni-YSZ electrode revealed by SEM is the formation of ZrO_2 nano-particles on Ni surfaces, which deteriorates the percolation of Ni and presumably decreases the number of active TPB. The degradation of Ni surface is a result of Ni-YSZ interfacial reactions, which are associated with the electrochemical processes and over-potential at the Ni-YSZ interface. A mechanism of how the ZrO_2 nano-particles are formed on Ni surfaces during the electrolysis cell testing is proposed. It is postulated that Zr is reduced at the Ni-YSZ interface, dissolved into Ni and precipitated as ZrO_2 at interfaces with higher $p(\text{O}_2)$. Relevant Ni-YSZ interfacial reactions and their likelihood under such conditions (T , $p(\text{O}_2)$) are further elucidated by thermodynamic calculations.

Acknowledgement

This work was financially supported by Energinet.dk through the projects ForskEL 2010-1-10432 “planSOEC-R&D and commercialization roadmap for SOEC electrolysis” and ForskEL 2011-1-10609 “Development of SOEC cells and stacks”.

References

- [1] A. Brisse, J. Schefold, and M. Zahid, *Int. J. Hydrogen Energy*, **33**, 5375 (2008).
- [2] S. D. Ebbesen, C. Graves, A. Hauch, S. H. Jensen, and M. Mogensen, *J. Electrochem. Soc.*, **157**, B1419 (2010).
- [3] Q. X. Fu, C. Mabilat, M. Zahid, A. Brisse, and L. Gautier, *Energy Environ. Sci.*, **3**, 1382 (2010).
- [4] C. Graves, S. D. Ebbesen, M. Mogensen, and K. S. Lackner, *Renewable Sustainable Energy Rev.*, **15**, 1 (2011).
- [5] A. Hauch, S. D. Ebbesen, S. H. Jensen, and M. Mogensen, *J. Electrochem. Soc.*, **155**, B1184 (2008).
- [6] R. Knibbe, M. L. Traulsen, A. Hauch, S. D. Ebbesen, and M. Mogensen, *J. Electrochem. Soc.*, **157**, B1209 (2010).
- [7] M. A. Laguna-Bercero, R. Campana, A. Larrea, J. A. Kilner, and V. M. Orera, *J. Power Sources*, **196**, 8942 (2011).
- [8] S. D. Ebbesen and M. Mogensen, *Electrochem. Solid-State Lett.*, **13**, B106 (2010).
- [9] A. Hagen, M. Menon, R. Barfod, P. V. Hendriksen, S. Ramousse, and P. H. Larsen, *Fuel Cells*, **6**, 146 (2006).
- [10] K. Thyden, Y. L. Liu, and J. B. Bilde-Sorensen, *Solid State Ionics*, **178**, 1984 (2008).
- [11] M. Chen, J. V. T. Høgh, J. U. Nielsen, J. J. Bentzen, S. D. Ebbesen, and P. V. hendriksen, *Fuel Cells*, accepted, (2013).

- [12] X. Sun, M. Chen, P. Hjalmarsson, S. D. Ebbesen, S. H. Jensen, M. Mogensen, and P. V. Hendriksen, *ECS Trans.*, **41**(33), 77 (2012).
- [13] P. Hjalmarsson, X. F. Sun, Y. L. Liu, and M. Chen, *J. Power Sources*, **223**, 349 (2013).
- [14] F. Tietz, D. Sebold, A. Brisse, and J. Schefold, *J. Power Sources*, **223**, 129 (2013).
- [15] T. Wagner, R. Kirchheim, and M. Ruhle, *Acta Metall. Mater.*, **40**, S85 (1992).
- [16] T. Wagner, G. Duscher, and R. Kirchheim, *J. Mater. Res.*, **14**, 3340 (1999).
- [17] D. Klotz, B. Butz, A. Leonide, J. Hayd, D. Gerthsen, and E. Ivers-Tiffée, *J. Electrochem. Soc.*, **158**, B587 (2011).
- [18] C. W. Bale, P. Chartrand, S. A. Degterov, G. Eriksson, K. Hack, R. Ben Mahfoud, J. Melancon, A. D. Pelton, and S. Petersen, *Calphad*, **26**, 189 (2002).
- [19] M. K. Dongare, K. Malshe, C. S. Gopinath, I. K. Murwani, and E. Kemnitz, *J. Catal.*, **222**, 80 (2004).
- [20] G. Dhalenne, B. Bonvalot, A. Revcolevschi, and F. Millot, *J. Am. Ceram. Soc.*, **73**, 1524 (1990).
- [21] A. C. Bose, R. Ramamoorthy, and S. Ramasamy, *Mater. Lett.*, **44**, 203 (2000).
- [22] M. W. Pitcher, S. V. Ushakov, A. Navrotsky, B. F. Woodfield, G. S. Li, J. Boerio-Goates, and B. M. Tissue, *J. Am. Ceram. Soc.*, **88**, 160 (2005).
- [23] W. S. Chang, S. Chen, and P. Shen, *Mater. Sci. Eng., A*, **145**, 113 (1991).
- [24] M. Kowalski and P. J. Spencer, *Calphad*, **19**, 229 (1995).
- [25] C. E. Campbell, W. J. Boettinger, and U. R. Kattner, *Acta Materialia*, **50**, 775 (2002).
- [26] J.-W. Park and C. Altstetter, *Metall. Trans. A*, **18**, 43 (1987).
- [27] M. Mezbahul-Islam and M. Medraj, *Calphad*, **33**, 478 (2009).
- [28] S. D. Ebbesen, R. Knibbe, and M. Mogensen, *J. Electrochem. Soc.*, **159**, F482 (2012).
- [29] S. D. Ebbesen and M. Mogensen, *ECS Trans.*, submitted, (2013).

[30] K. V. Hansen, K. Norrman, and M. Mogensen, *Surf. Interface Anal.*, **38**, 911 (2006).

Table 1 Test conditions of the studied cells [5, 11-13]. Theoretical EMF values at these test conditions are included as well for comparison.

Cell ID in the present work	Test type	Conditions for galvanostatic durability tests									
		Tem p. (°C)	Gas composition (to Ni/YSZ)	Current density (A/cm ²)	Gas (CO ₂ +H ₂ O) conversion (%)	Testing period (hour)	Theoretic al EMF (mV)	Measur ed OCV (mV)	Final cell voltage ^a (mV)	Final cell over-potential ^a (mV)	ΔV ^b (mV)
A1	Durability	800	CO ₂ /H ₂ O/H ₂ (45/45/10)	-1.5	62%	312	874	872	1772	900	300
A2	Durability	800	CO ₂ /H ₂ O/H ₂ (45/45/10)	-1.5	62%	584	874	870	1703	833	242
A3	Durability	800	CO ₂ /H ₂ O/H ₂ (45/45/10)	-1.5	62%	526	874	870	1694	824	265
A4	Durability	850	CO ₂ /H ₂ O/H ₂ (45/45/10)	-1	62%	1256	853	863	1283	420	153
A5	Durability	850	H ₂ /H ₂ O (50/50)	-1.5	80%	890	962	961	1873	912	413
A6	Durability	800	CO ₂ /H ₂ O/H ₂ (45/45/10)	-0.75	60%	1005	874	875	1204 ^c 1129 ^d	329 ^c 254 ^d	-118
A7	Durability	850	H ₂ /H ₂ O (50/50)	-0.5	28%	1316	962	953	1175	222	32
A8	Durability	850	H ₂ /H ₂ O (50/50)	-0.5	28%	1510	962	955	1116	161	41
Ref1	Only initial performance characterization, no durability test.										
Ref2	Only initial performance characterization, no durability test.										

^a Measured at the end of the durability tests at the conditions for the long-term testing.

^b ΔV = (Cell Voltage)_{End} – (Cell voltage)_{Start}

^c Over the entire SRU (single repeat unit).

^d Over the cell, i.e. corrected with voltage loss due to interconnect plate contact resistance (about 75 mV).

Table 2 Summary of main findings from post-mortem characterizations of the Ni/YSZ electrodes

Cell ID in the present work	Conditions for galvanostatic durability tests			Fractured surface	Polished surface	
	Current density (A/cm ²)	Temp. (°C)	Final cell over-potential ^a (mV)	Number of ZrO ₂ nano-particles per Ni grain	Loss of Ni percolation	Formation of gaps or new phases at the Ni-Ni or Ni-YSZ interface
A1	-1.5	800	900	(Not examined)	Severe	Yes
A2	-1.5	800	833	Up to a few tens	(Not examined)	Yes
A3	-1.5	800	824	Up to a few tens	(Not examined)	Yes
A4	-1	850	420	Up to a few hundred	(Not examined)	Yes
A5	-1.5	850	912	(Not examined)	Most severe	Yes
A6	-0.75	800	329 ^b 254 ^c	(Not examined)	Minor	No
A7	-0.5	850	222	0	(Not examined)	No
A8	-0.5	850	161	0	(Not examined)	No
Ref1				(Not examined)	Negligible	No
Ref2				0	(Not examined)	No

^a Measured at the end of the durability tests at the conditions for the long-term testing.

^b Over the entire SRU (single repeat unit).

^c Over the cell, i.e. corrected with voltage loss due to interconnect plate contact resistance (about 75 mV).

Table 3 EDS point analysis within Ni in the active Ni/YSZ electrode layer in Cell A5 (-1.5 A/cm², 850 °C).

	Zr, at. %	Si, at. %
Ni grains at the electrode-electrolyte interface		
No. 1	3.7	3.8
No. 2	5.8	3.8
No. 3	3.7	1.8
No. 4	2.8	2.0
Ni grains 2-3 μm from the interface		
No. 1	5.9	~ 0
No. 2	1.7	0.7
No. 3	3.7	~ 0
No. 4	2.9	~ 0

Figure captions:

Figure 1 Development of the cell voltages with time under galvanostatic conditions. The detailed test conditions are listed in Table 1. The voltage fluctuation for Cell A1 within the first 70 hours was caused by unstable steam supply, which was later resolved for the remaining test period. The voltage for Cell A6 was measured over the SRU (single repeat unit, including cell, interconnect, and contact between the cell and interconnect). The actual cell voltage is about 75 mV lower than the measured SRU voltage.

Figure 2 Fracture surface of (a) Cell A3 (-1.5 A/cm^2 , 800°C), (b), (c), and (d) of Cell A4 (-1 A/cm^2 , 850°C) showing nano-particles formed on the surface of Ni grains right at the interface with the electrolyte, (e) Cell A8 (-0.5 A/cm^2 , 850°C) and (f) Cell Ref2 showing the surface of Ni grains is free of nano-particles. For Cell A4, the SEM images were taken from the inlet (Figure 2b), center (Figure 2c), and outlet (Figure 2d), respectively. For all the other cells, the images presented were taken from the center.

Figure 3 EDS point analyses on Ni and YSZ grain surfaces of the fractured samples from a) Cell A4 (-1 A/cm^2 , 850°C) and b) Cell Ref2. The results show qualitatively that the nano-particles observed in Cell A4 contain Zr and O.

Figure 4 (a) TEM image showing morphology of the Ni-YSZ interface in Cell A4. (b) and (c) HRTEM images of the circled areas of nano-particles. The insets are the enlarged local IFFT images. (d) EDS point analysis of the characteristic areas of Points 1-3 in Figure 4a.

Figure 5 SEM images showing Ni percolation in the active Ni/YSZ electrode and in the support layer (a) Cell A1 (-1.5 A/cm^2 , 800°C), (b) Cell A5 (-1.5 A/cm^2 , 850°C), (c) Cell A6 (-0.75 A/cm^2 , 800°C) and (d) Cell Ref1.

Figure 6 SEM images of the active Ni/YSZ electrode (a) Cell A1 (-1.5 A/cm^2 , 800°C), (b) Cell A5 (-1.5 A/cm^2 , 850°C), (c) Cell A6 (-0.75 A/cm^2 , 800°C), (d) Cell A8 (-0.5 A/cm^2 , 850°C), and (e) Cell Ref1.

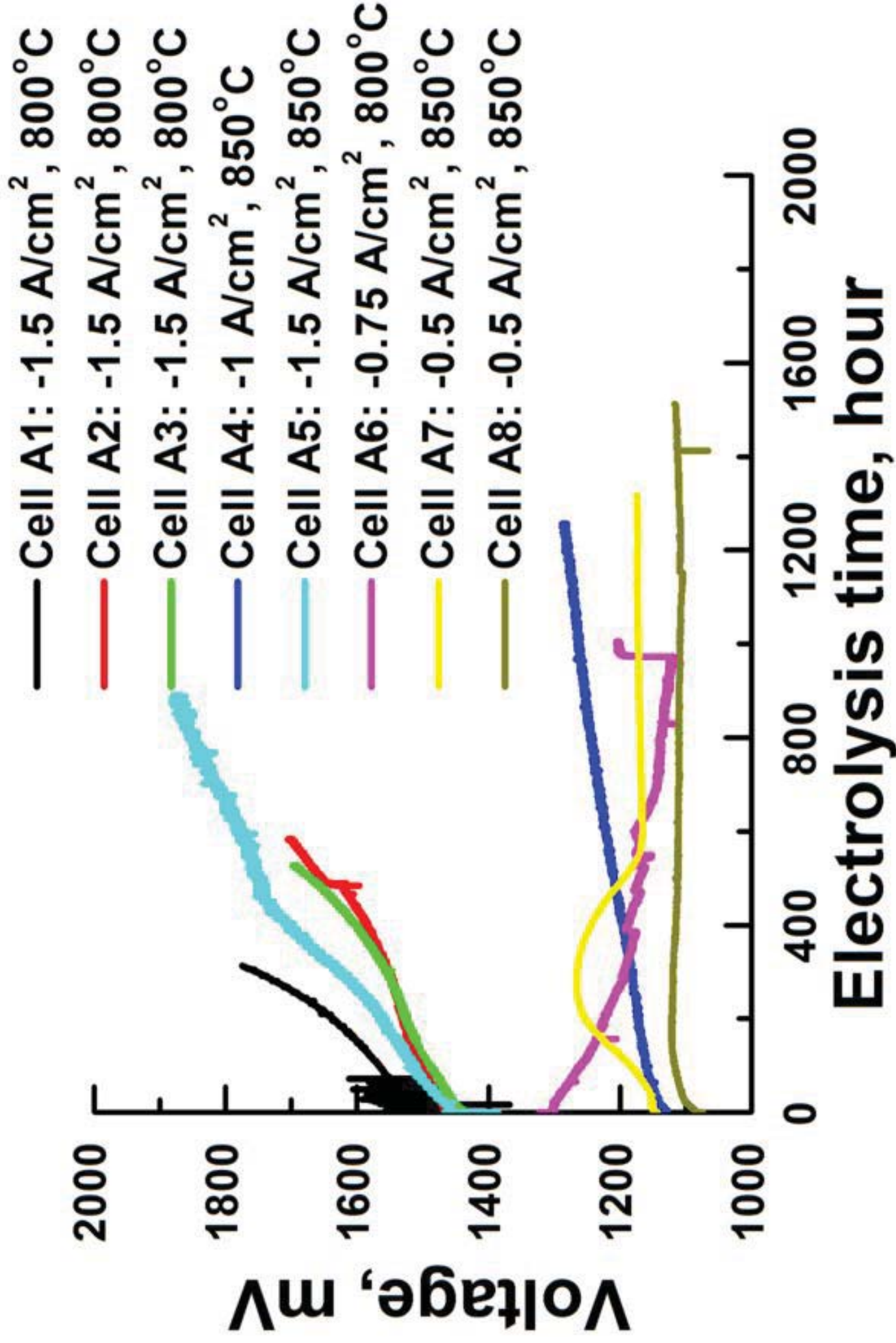
Figure 7 (a) SEM image and (b) EDS linescan of Cell A5 (-1.5 A/cm^2 , 850°C).

Figure 8 Schematic illustration of the mechanism for formation of ZrO_2 nano-particles on Ni surfaces.

Figure 9 Phase diagram of Ni-Zr- O_2 at 850°C .

Figure 10 Ni-rich part of Ni-Zr- O_2 phase diagram at 850°C .

Figure 11 Over-potential of the Ni-YSZ interface, (a) Cell A5 (-1.5 A/cm^2 , 850°C), (b) Cell A8 (-0.5 A/cm^2 , 850°C). In each figure, the $p(\text{O}_2)$ value at the bottom corresponds to that of gas at zero conversion, while the three $p(\text{O}_2)$ values at the top correspond to $p(\text{O}_2)$ ranges for Reaction (1).

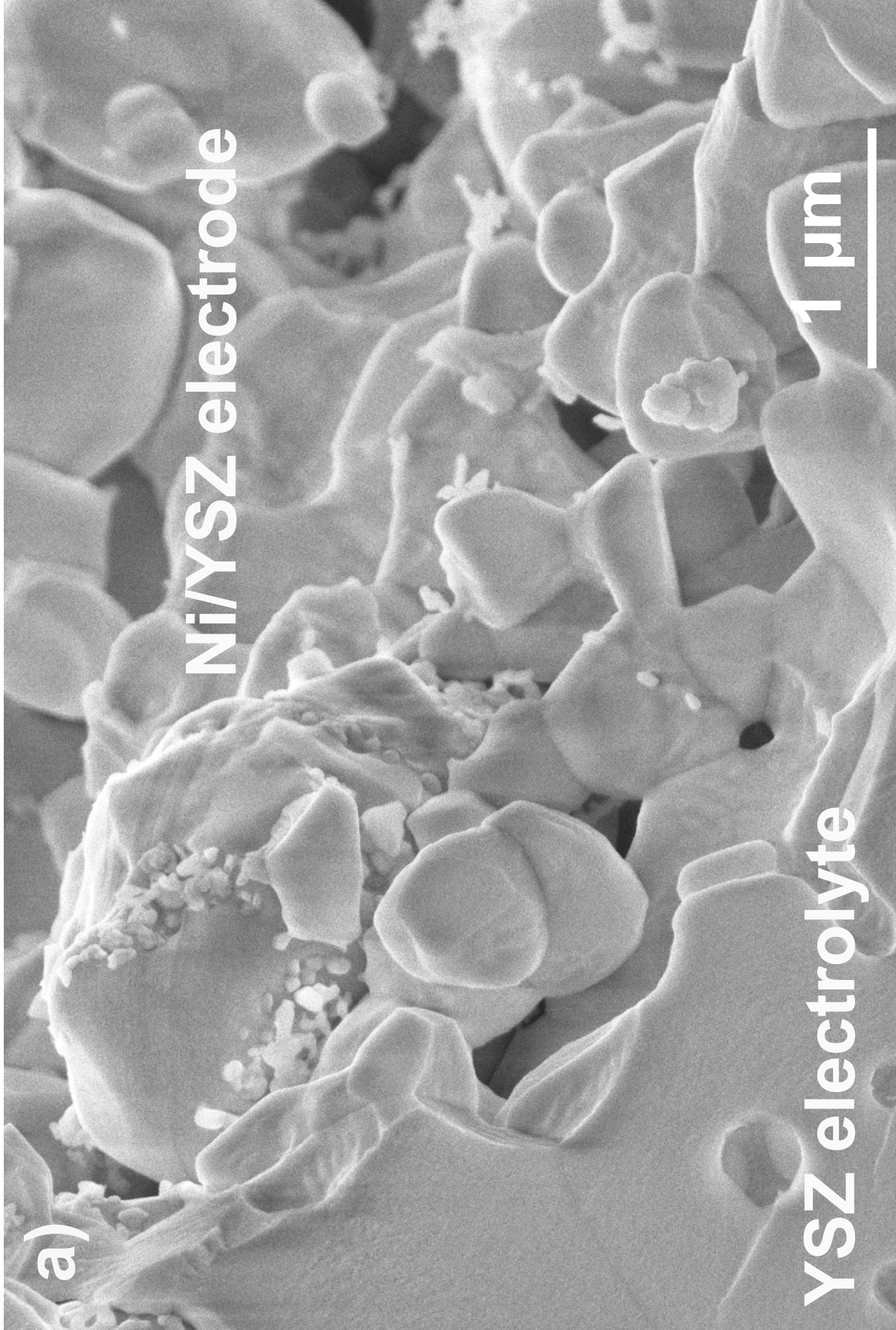


a)

Ni/YSZ electrode

YSZ electrolyte

1 μm

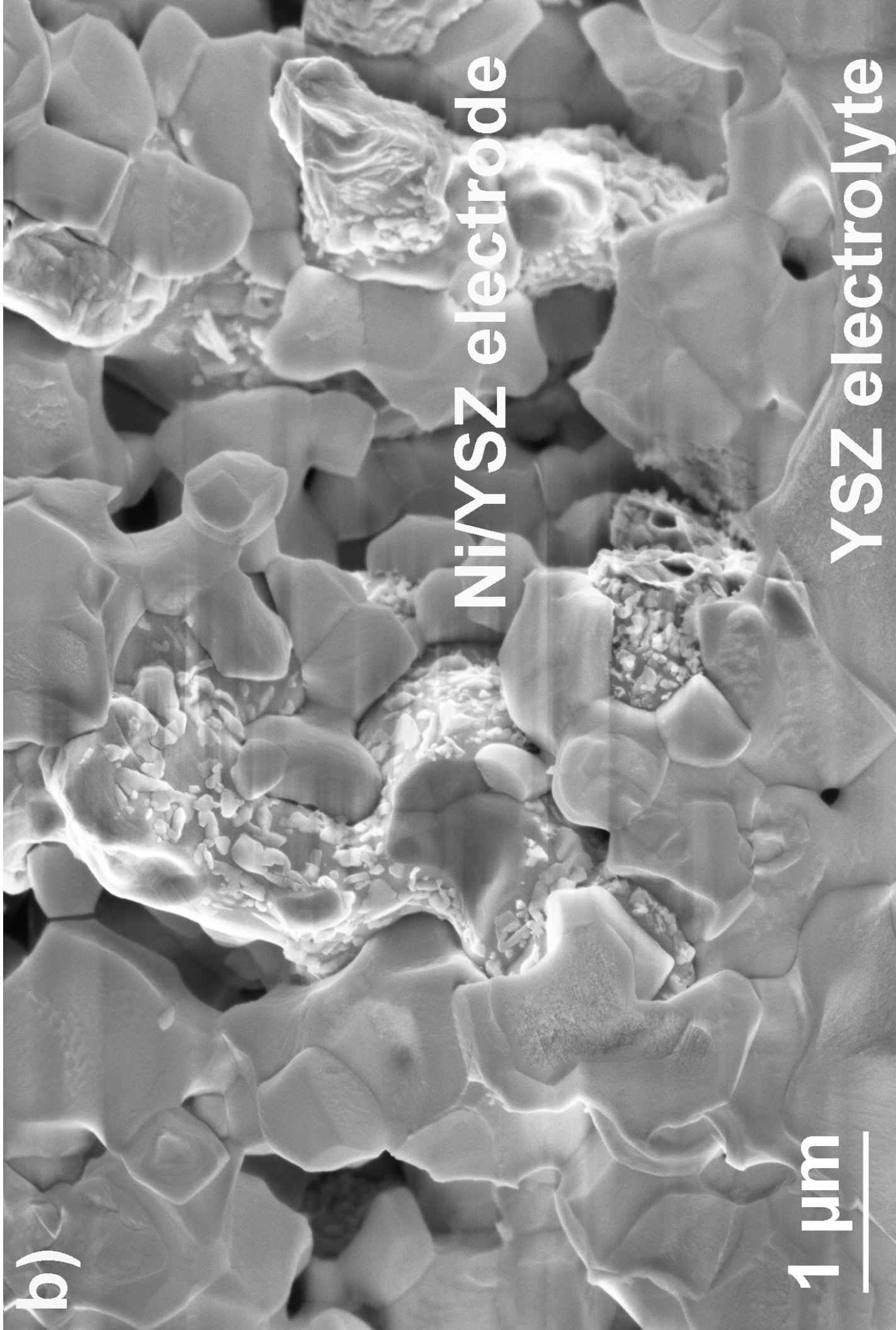


b)

Ni/YSZ electrode

YSZ electrolyte

1 μm



c)

Ni/YSZ electrode

YSZ electrolyte

1 μm



d)

Ni/YSZ electrode

YSZ electrolyte

200 nm

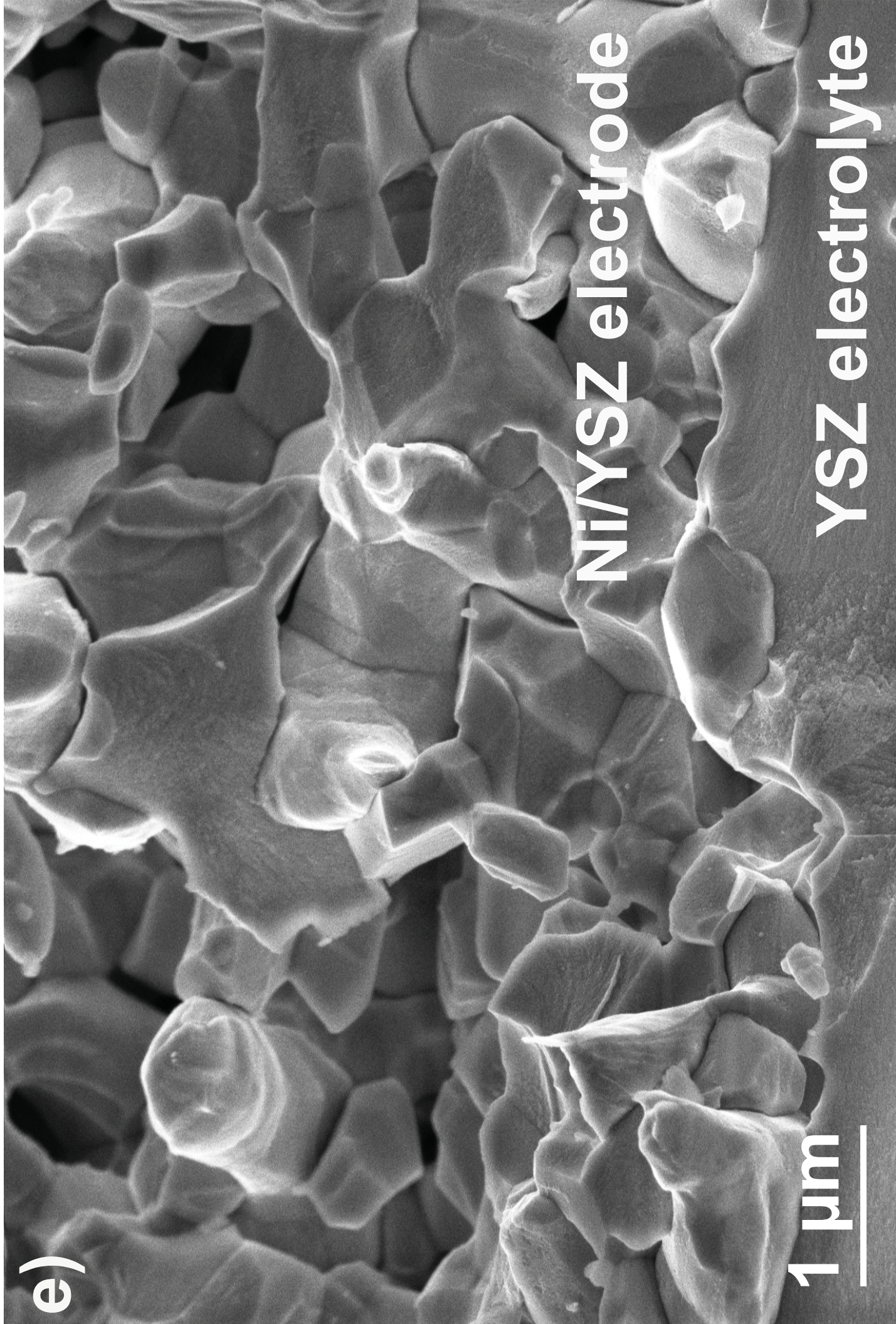


e)

Ni/YSZ electrode

YSZ electrolyte

1 μm

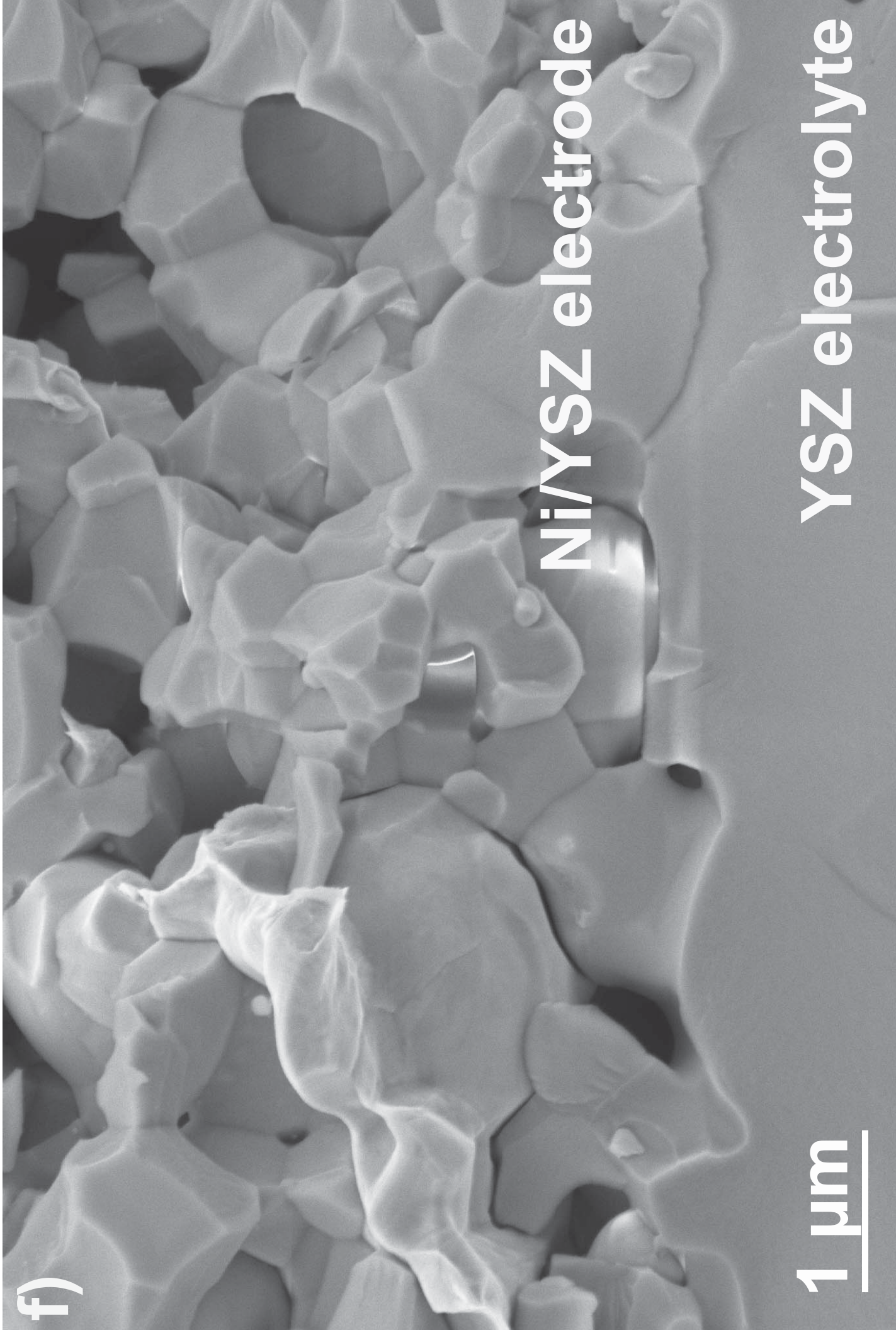


f)

Ni/YSZ electrode

1 μm

YSZ electrolyte



YSZ electrolyte

Ni/YSZ electrode

a)

3

2

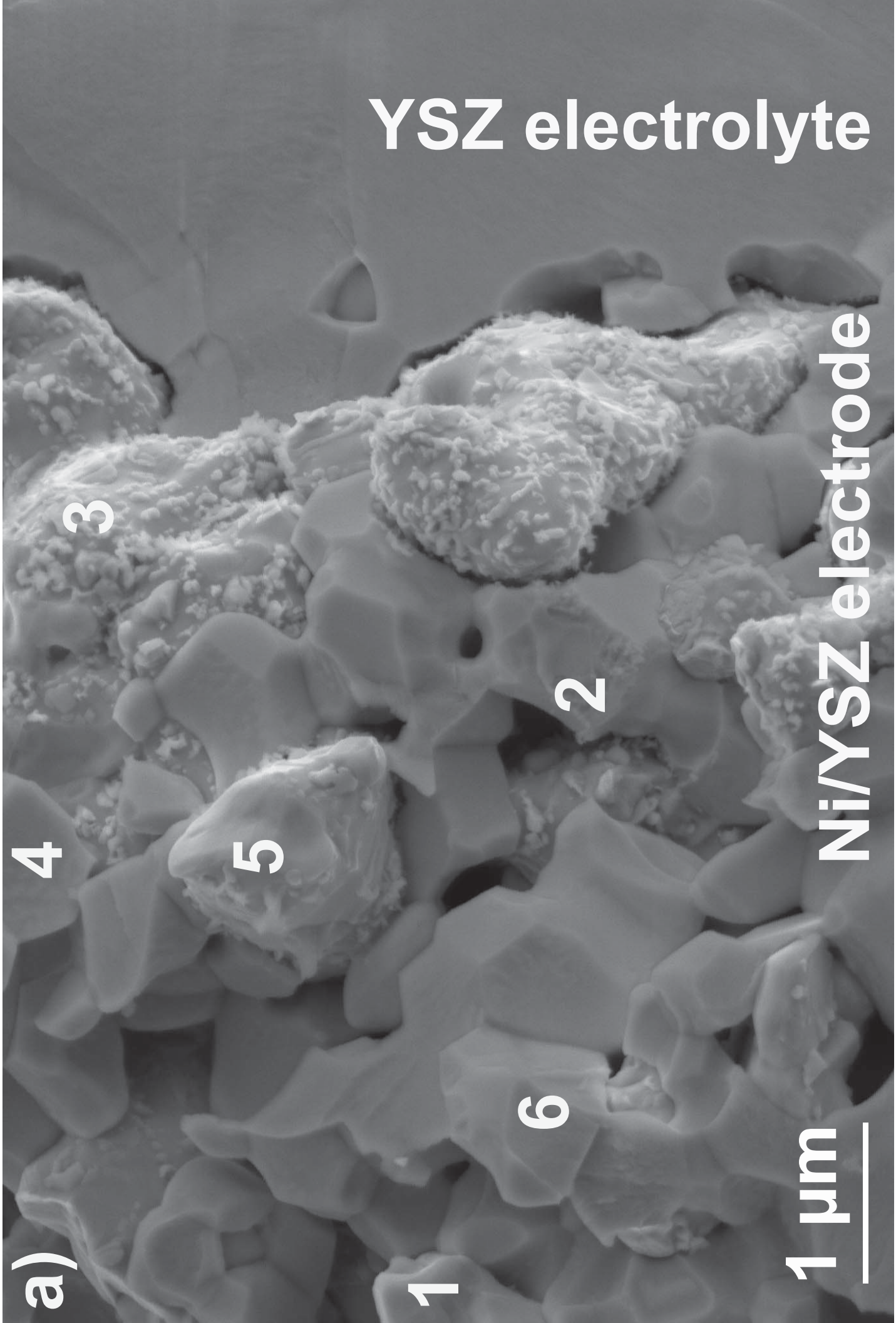
5

6

1

4

1 μm



	O, at. %	Ni	Y	Zr	Hf
Point 1	6.4	92.5	0.0	1.0	0.1
Point 2	65.2	0.6	5.9	27.8	0.5
Point 3	29.1	57.2	2.2	11.5	0.0
Point 4	62.6	1.8	6.3	28.9	0.4
Point 5	9.6	87.5	0.7	2.2	0.0
Point 6	68.1	0.7	5.6	25.4	0.2

b)

3

Ni/YSZ electrode

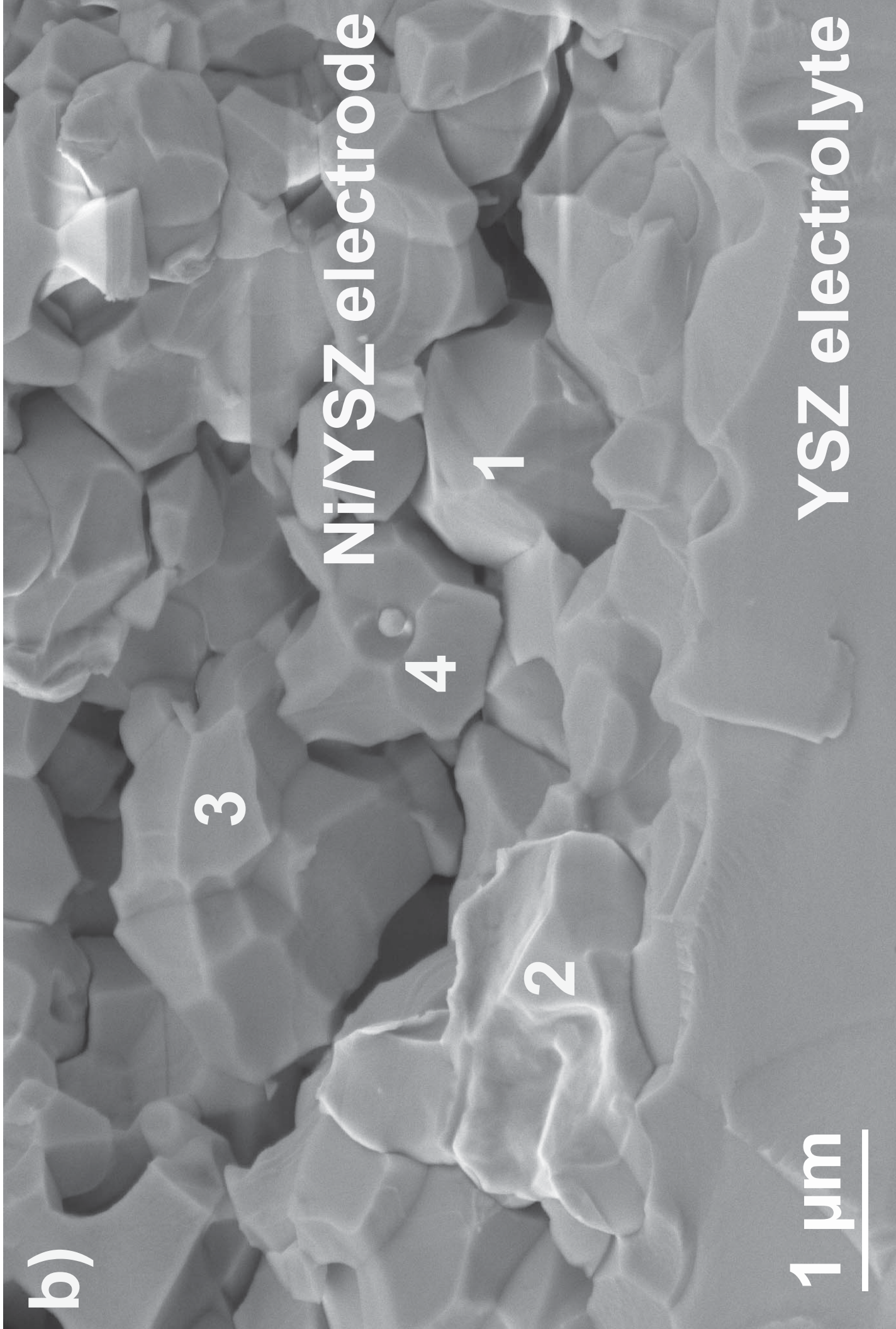
4

1

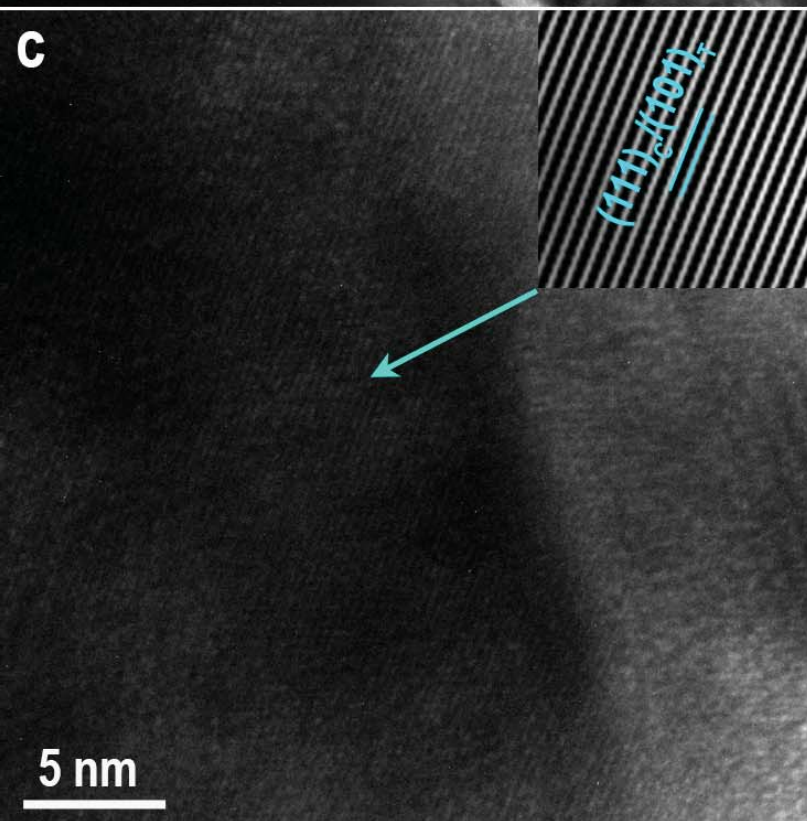
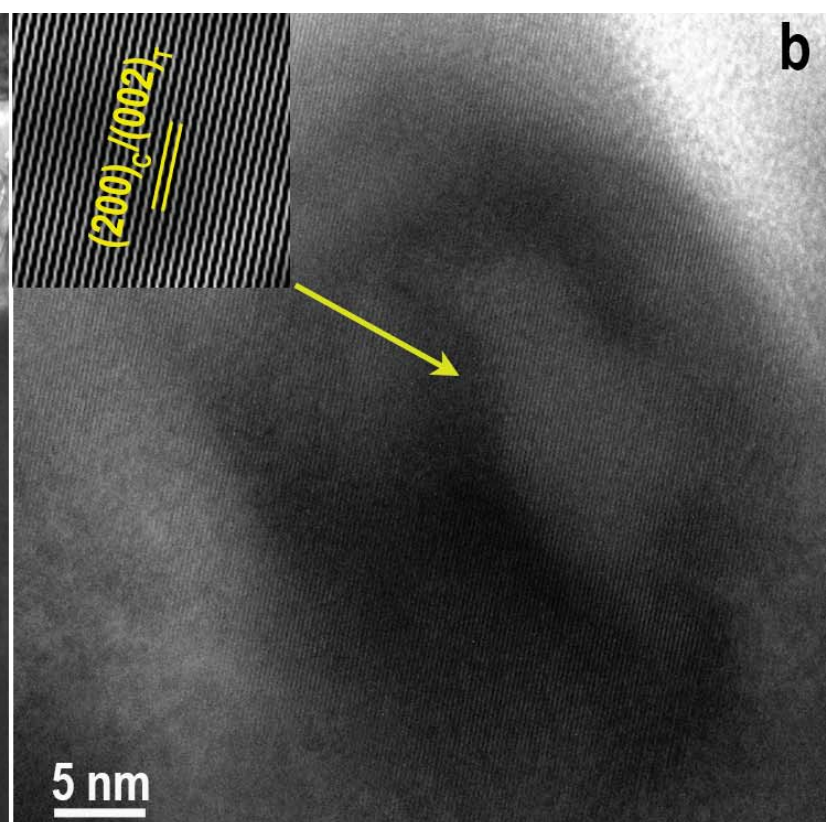
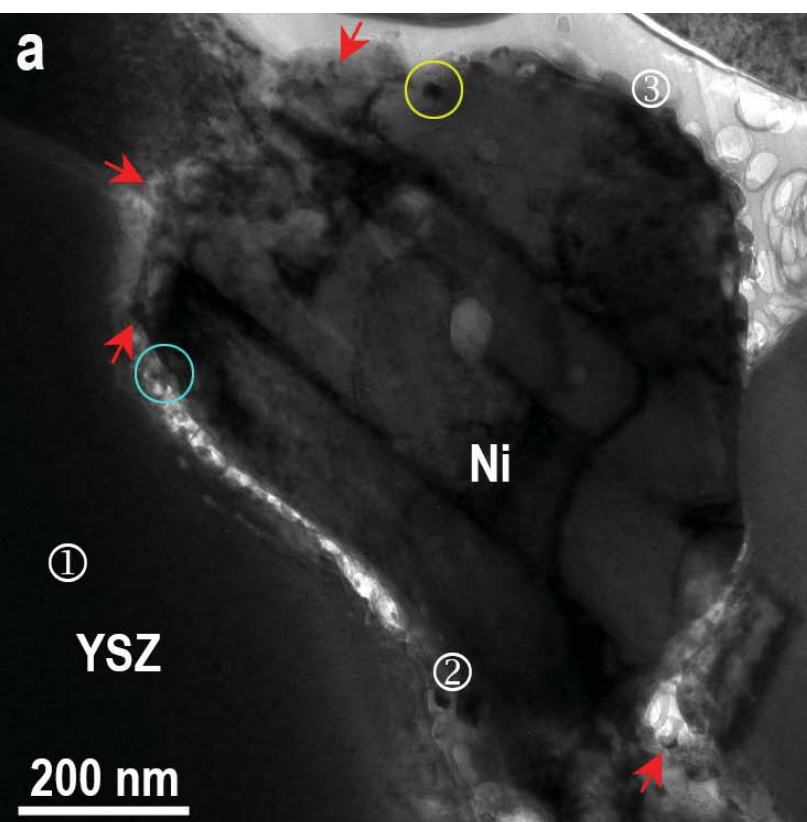
2

1 μm

YSZ electrolyte



	O, at.%	Ni	Y	Zr	Hf
Point 1	10.3	87.4	0.3	1.9	0.1
Point 2	7.0	91.7	0.3	0.7	0.3
Point 3	73.0	0.0	5.6	21.1	0.3
Point 4	64.5	0.0	5.0	30.3	0.2



d

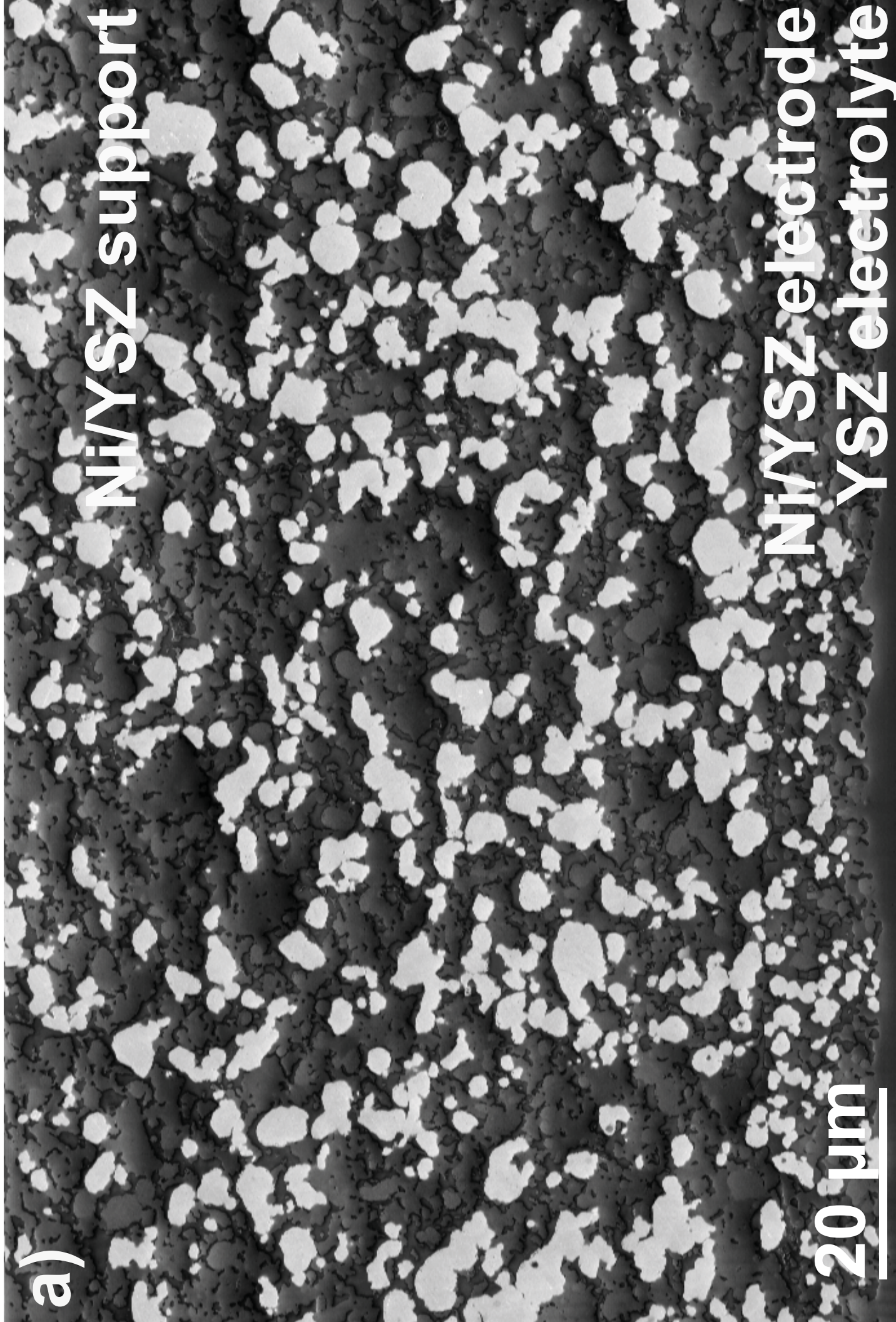
	Ni, cation%	Y	Zr
Point ①	2.1	18.4	79.5
Point ②	15.9	22.0	62.1
Point ③	9.9	12.2	77.9

a)

Ni/YSZ support

Ni/YSZ electrode
YSZ electrolyte

20 μm

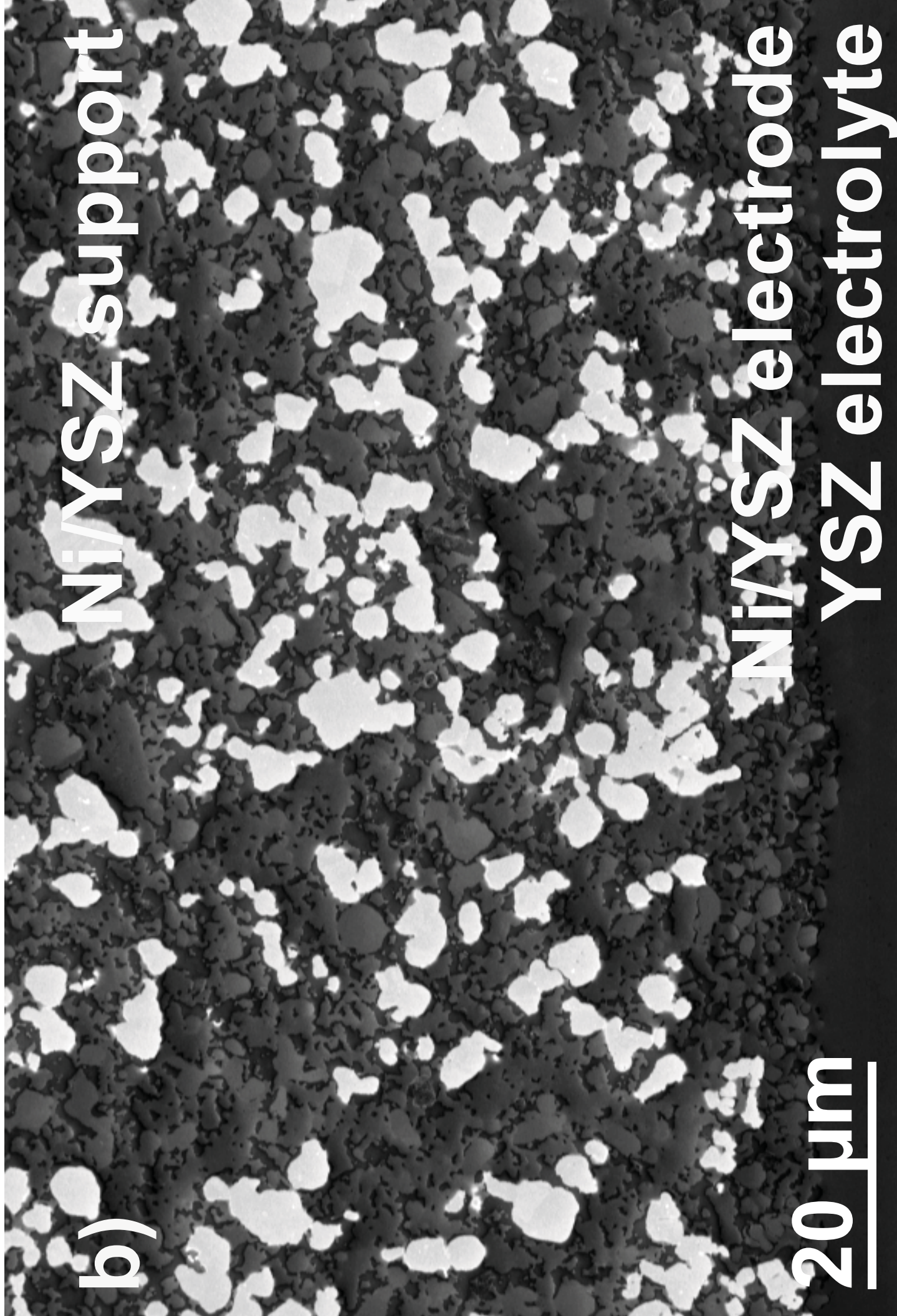


b)

Ni/YSZ support

Ni/YSZ electrode
YSZ electrolyte

20 μm

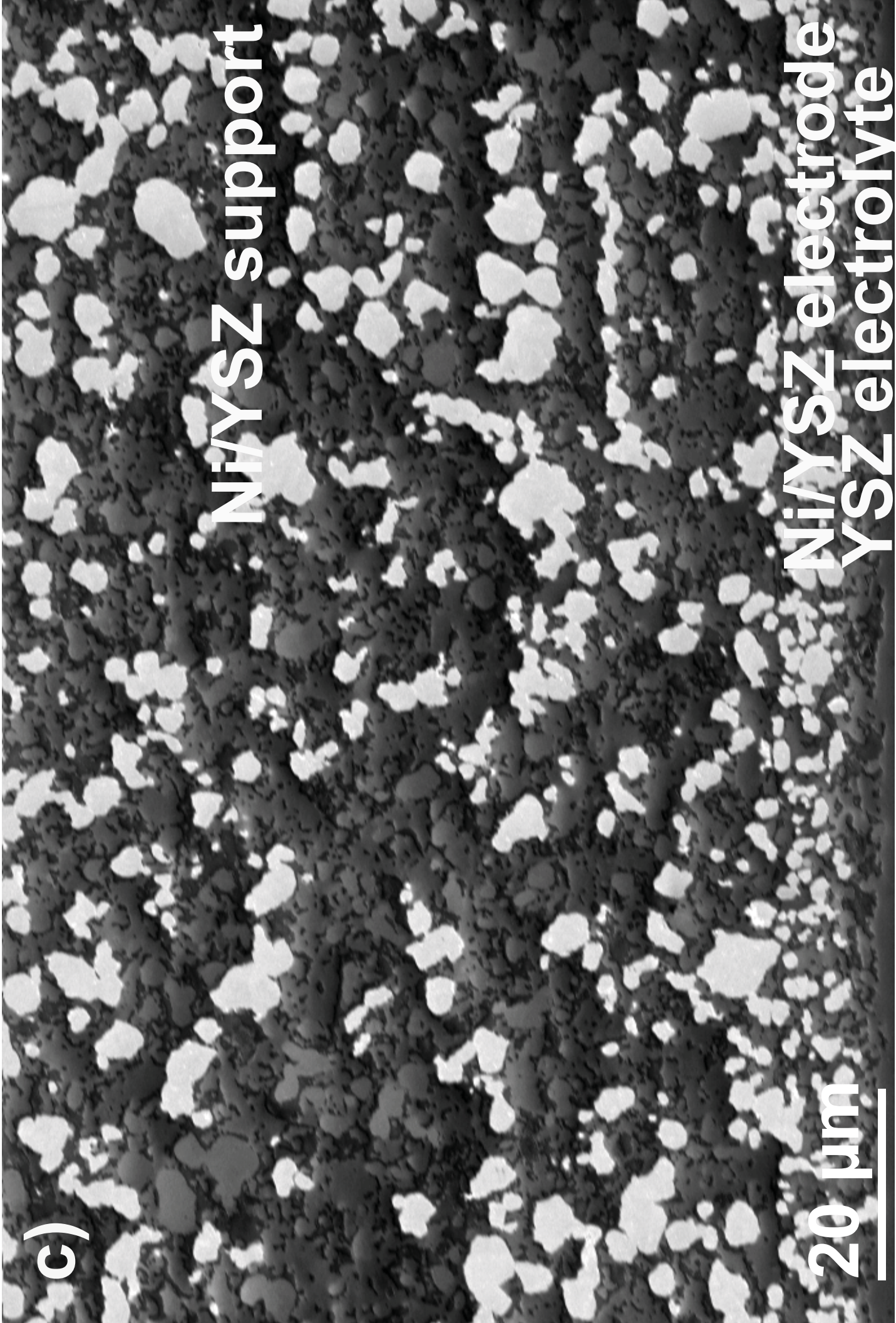


c)

Ni/YSZ support

Ni/YSZ electrode
YSZ electrolyte

20 μm



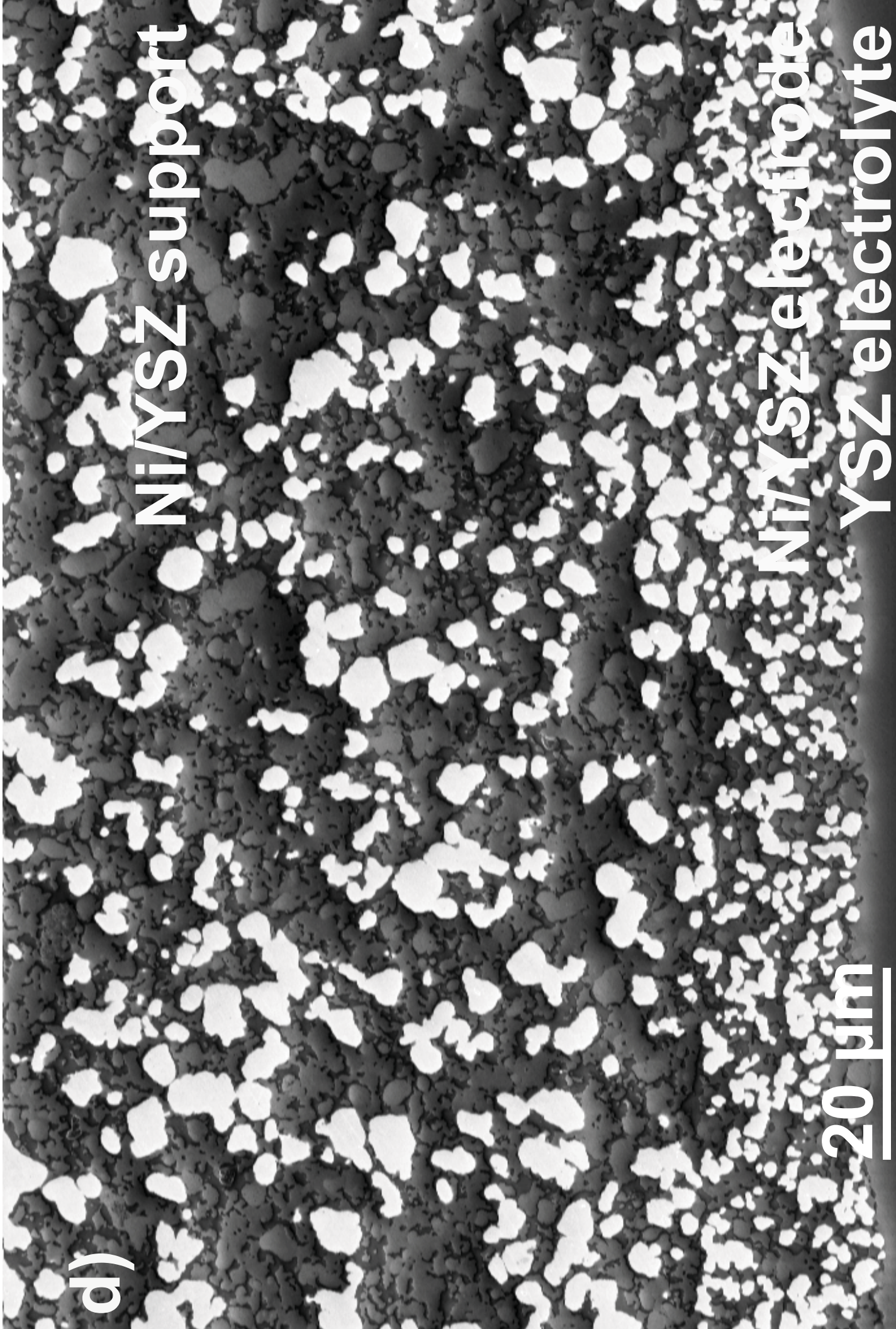
d)

Ni/YSZ support

Ni/YSZ electrode

YSZ electrolyte

20 μm

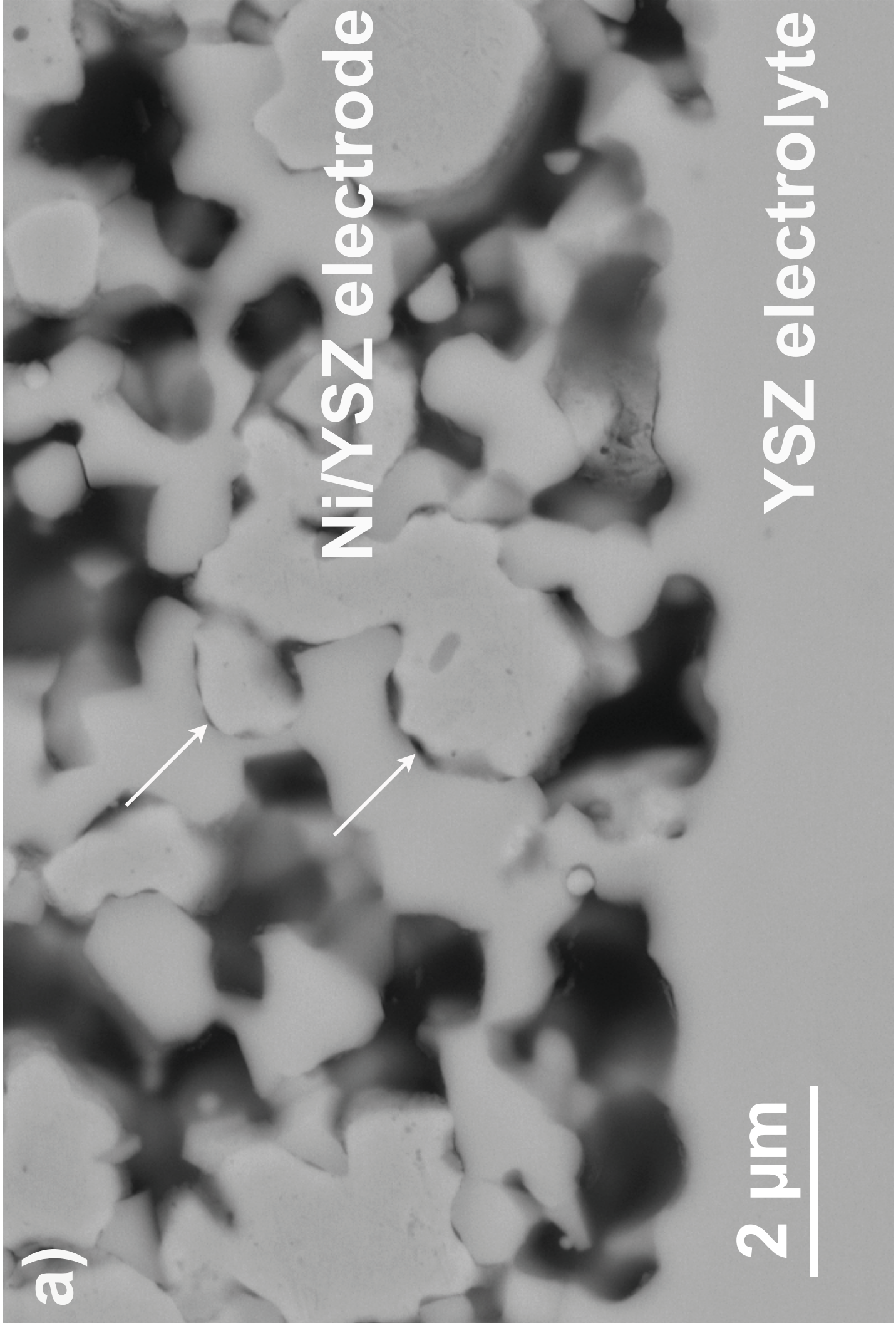
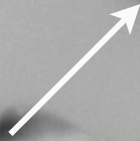


a)

Ni/YSZ electrode

YSZ electrolyte

2 μm

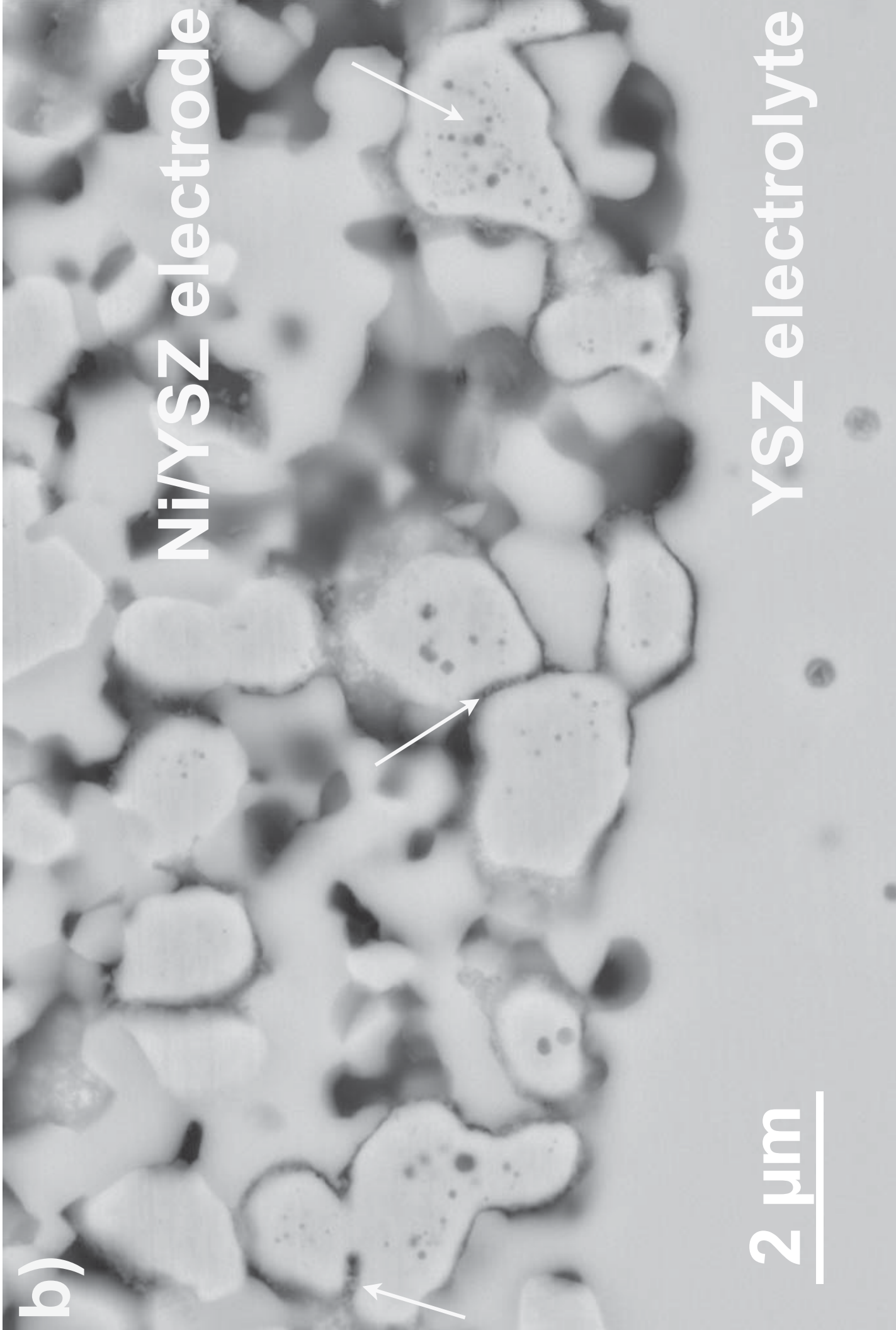


(b)

Ni/YSZ electrode

2 μm

YSZ electrolyte

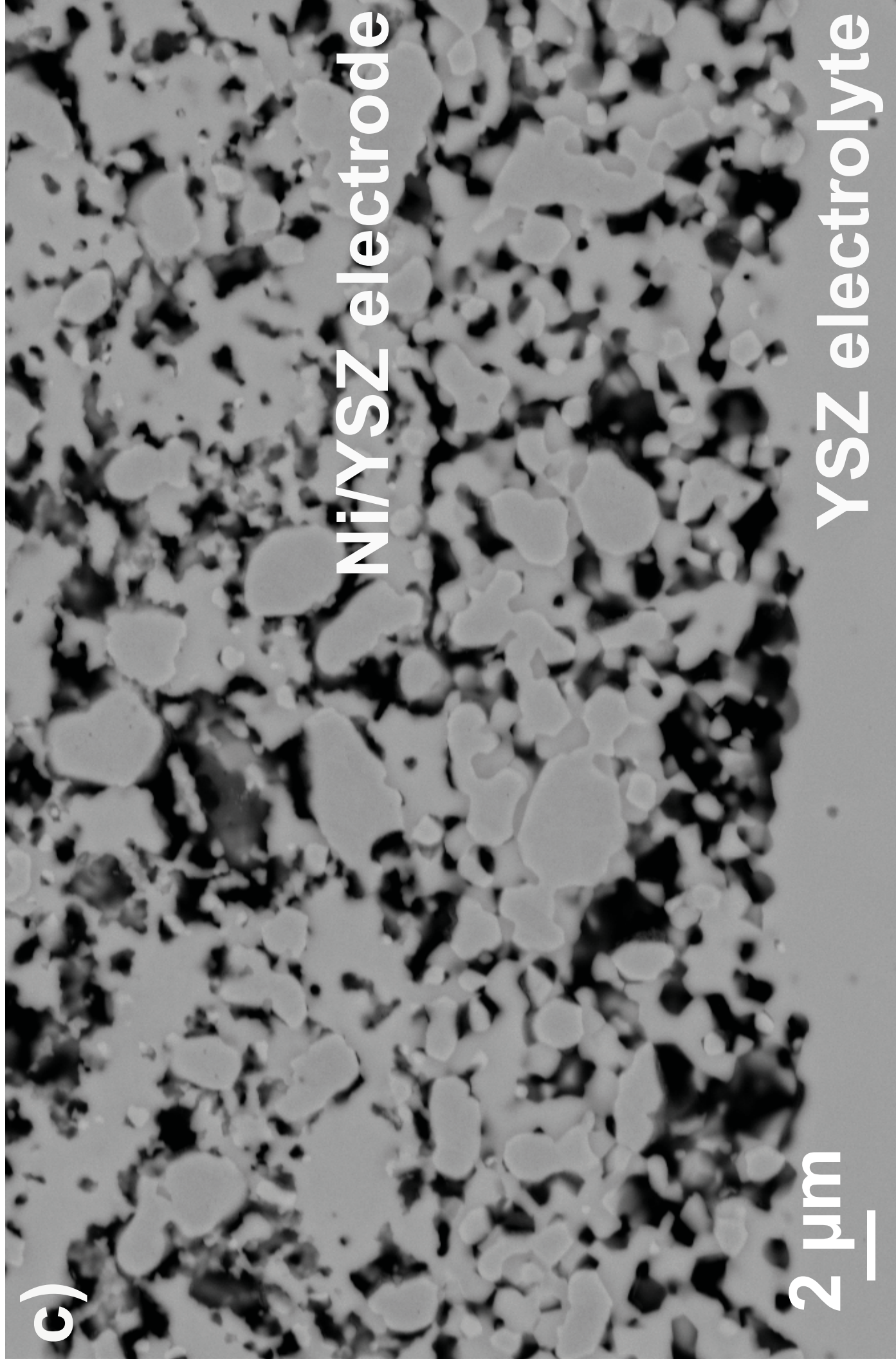


c)

Ni/YSZ electrode

2 μm

YSZ electrolyte

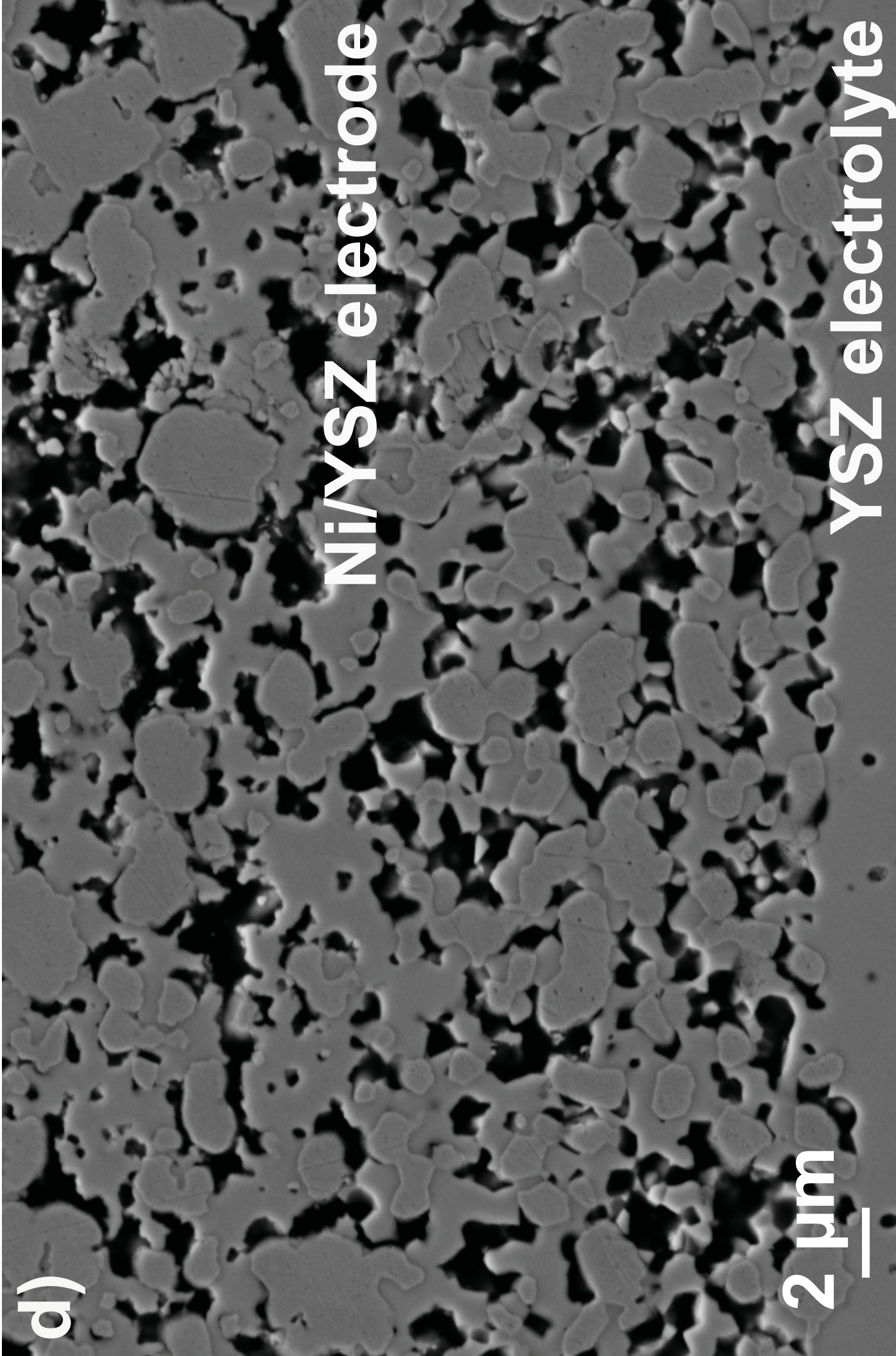


d)

Ni/YSZ electrode

2 μm

YSZ electrolyte



e)

Ni/YSZ electrode

2 μm

YSZ electrolyte

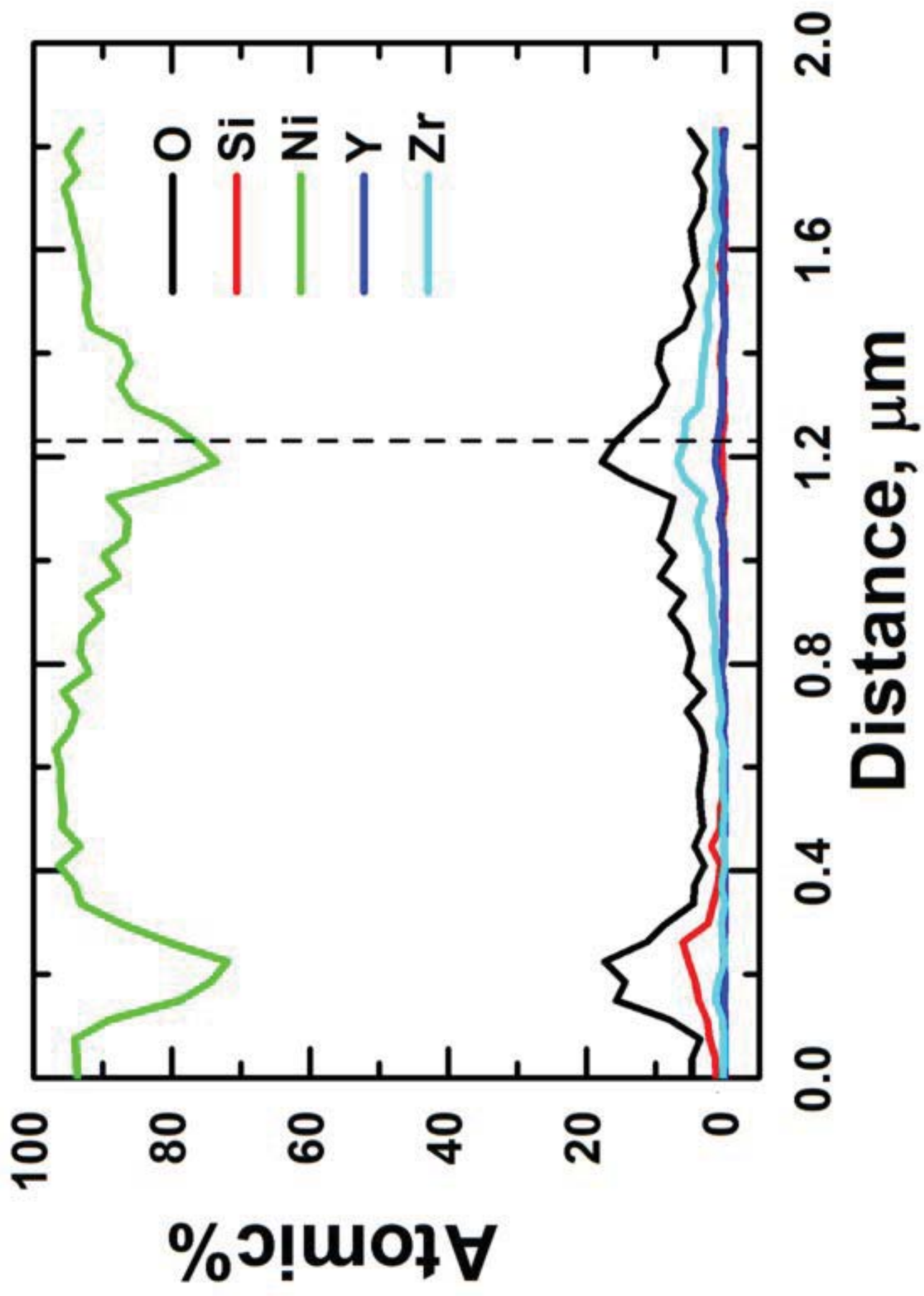


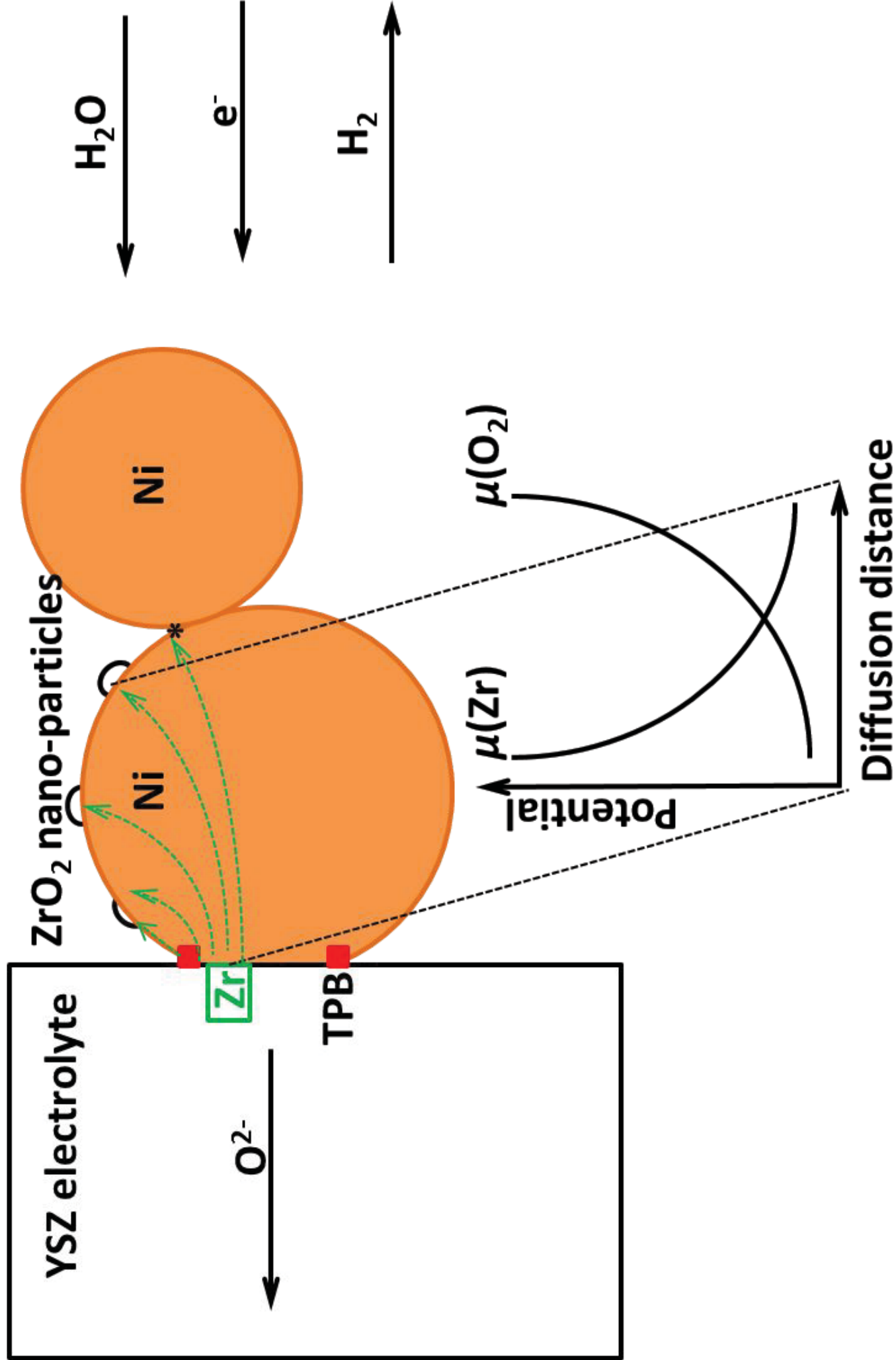
YSZ electrolyte

Ni/YSZ electrode

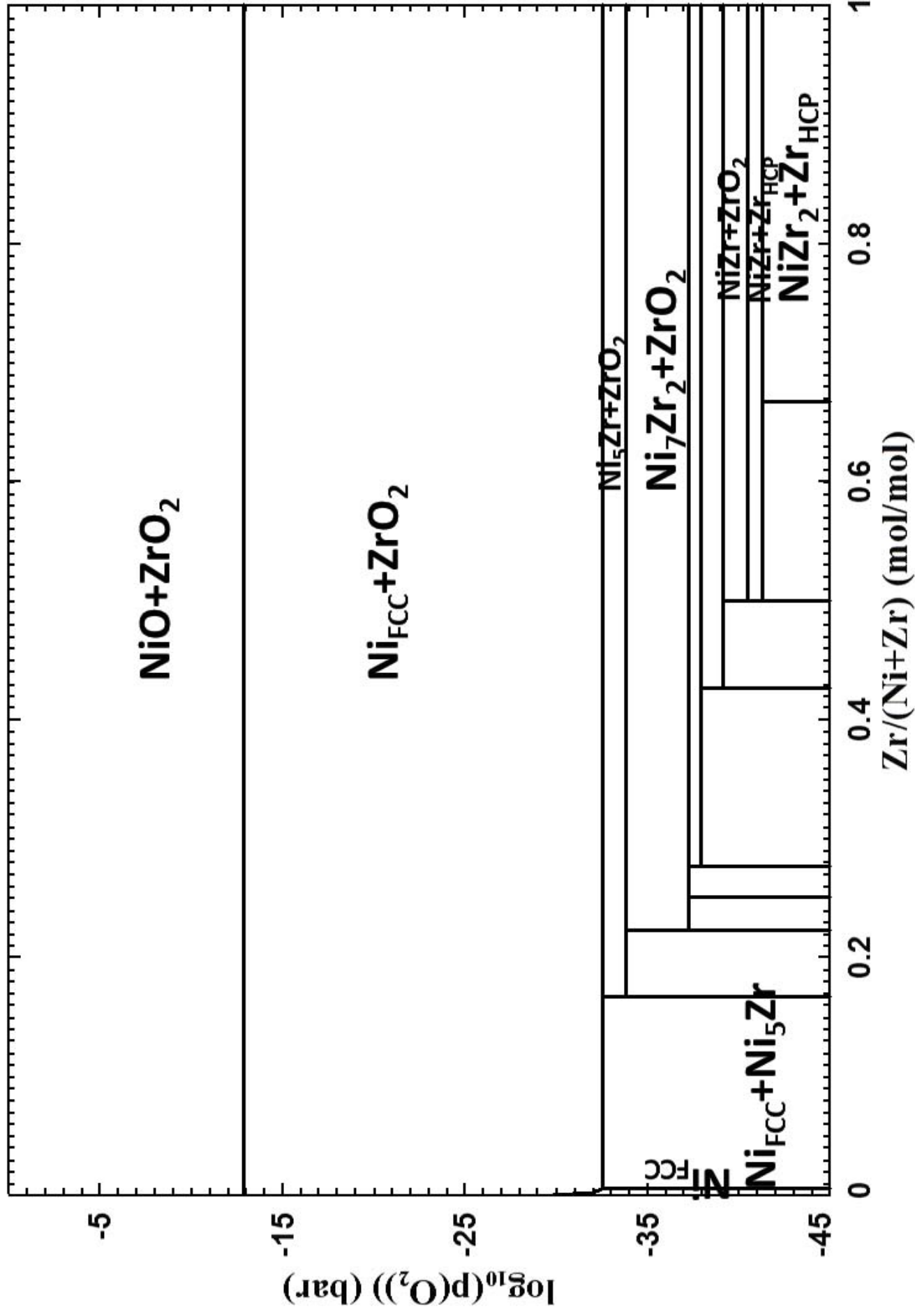
2 μ m



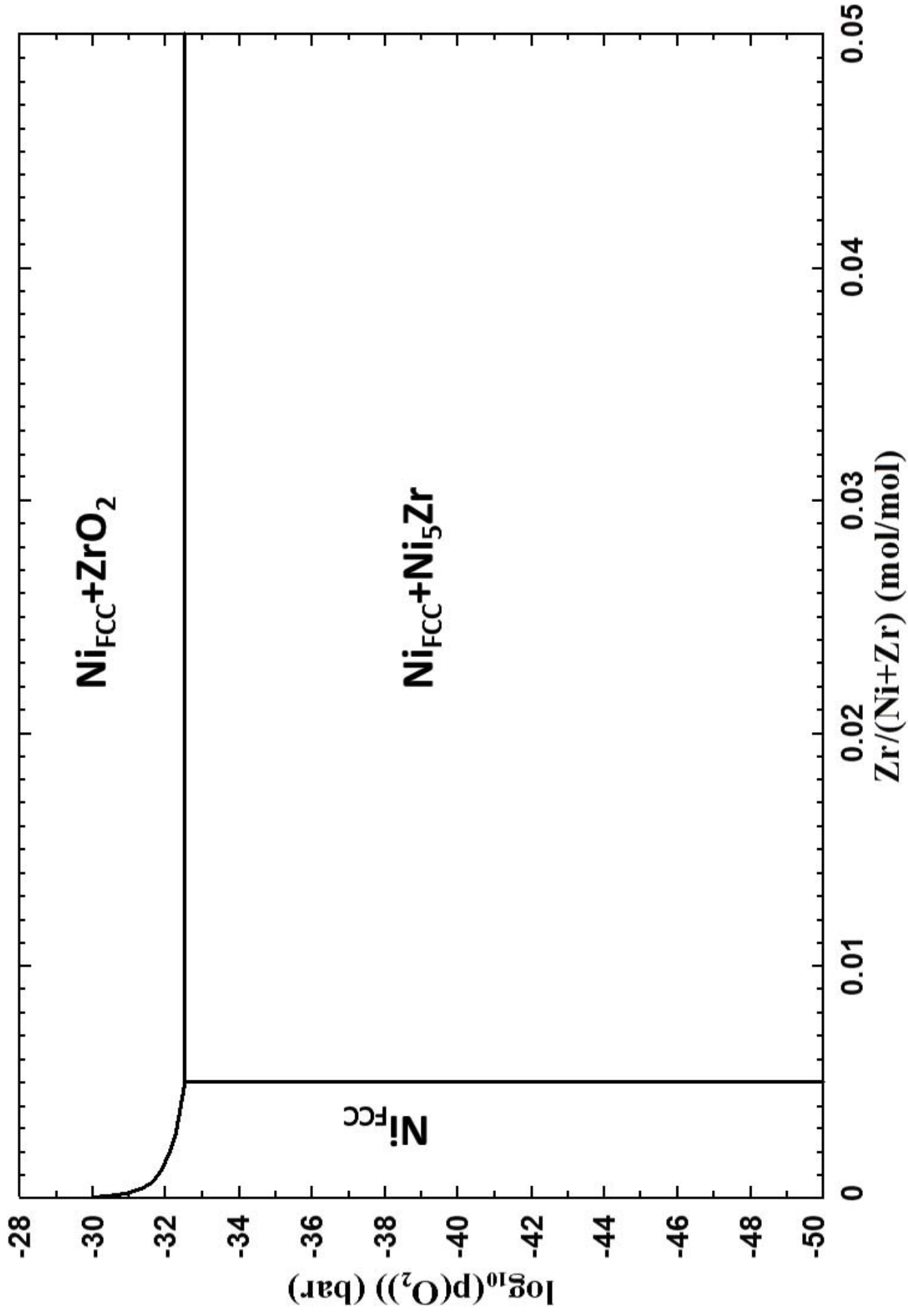




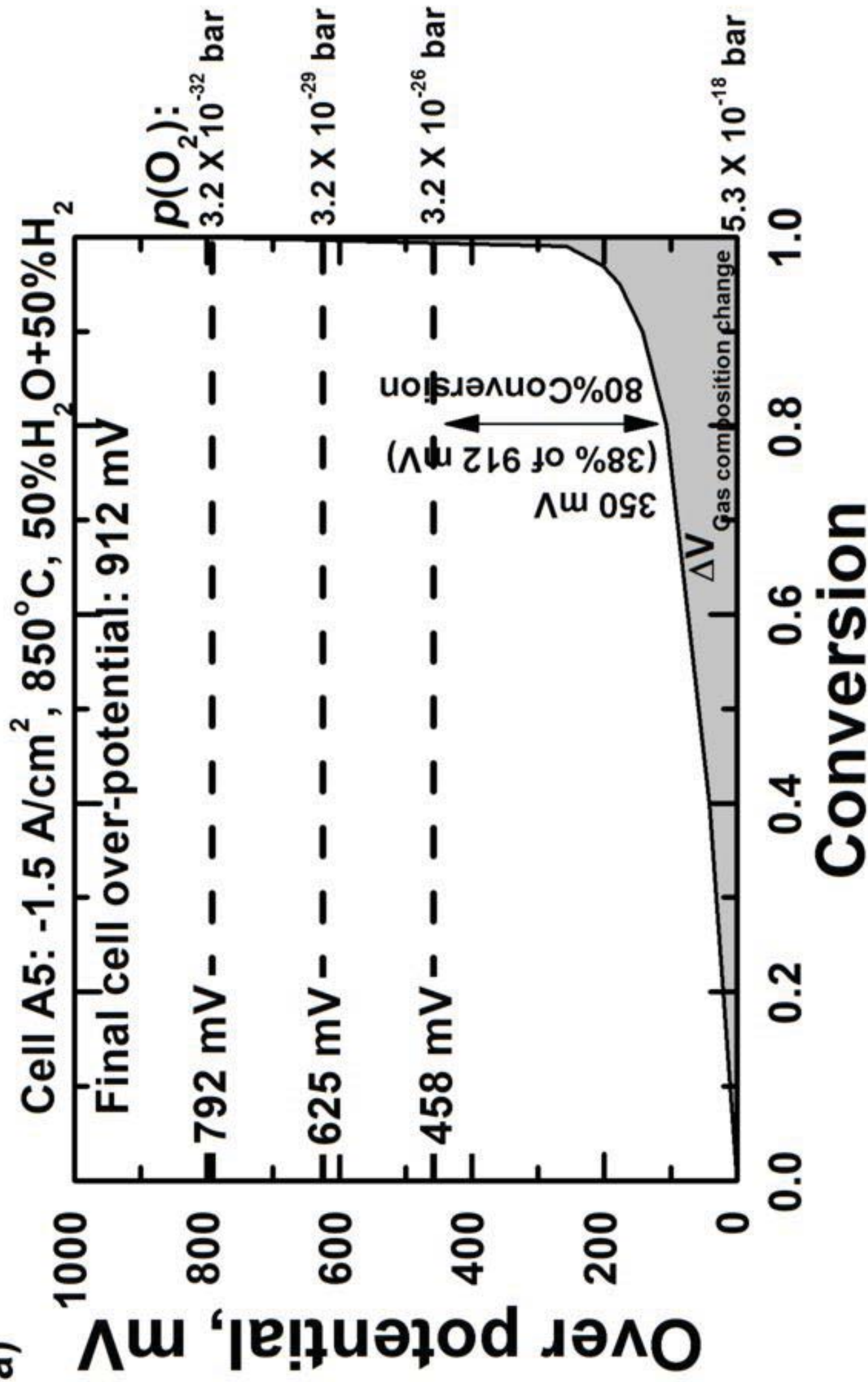
Ni - Zr - O₂
850°C



Ni - Zr - O₂
850°C



a)



b)

